Oklahoma State University

Stillwater, Oklahoma



Facilities Management - Energy Services Central Plant, Bldg. #0282 – 510 North Washington, Stillwater OK 74078

Distribution Systems Utilities Distribution **Natural Gas System** Operations & Maintenance Manual

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INTRODUCTION

The purpose of this OSU Natural Gas O&M Manual is to establish policies and procedures that conform to federal and state safety regulations for the installation, construction, maintenance, and operation of natural gas distribution facilities on the Oklahoma State University, Stillwater campus (OSU). This Manual contains the guidelines, practices, and procedures that assure OSU operates in compliance with accepted gas distribution and pipeline safety codes.

This manual is compiled from current federal and state regulatory documents for the exclusive use and application by OSU, Facilities Management (FM) personnel. <u>Any use or application to gas operations at other locations will be at self-risk to the user.</u>

The Natural Gas Pipeline Safety Act of 1968 required the United States Department of Transportation (DOT) to develop and enforce minimum safety regulations for the transportation of gases by pipeline. These regulations first became effective in 1970, and the *Research and Special Programs Administration* of DOT is charged with their enforcement. They are published in Title 49 of the *Code of Federal Regulations* (CFR), Parts 190, 191, 192, and 199. On December 4, 2009, the *Pipeline and Hazardous Materials Safety Administration* (PHMSA) published the final *Distribution Integrity Management Programs* (DIMP) rule. The rule required each operator of a natural gas utility, master meter system or propane pipeline system to prepare and follow a written DIMP plan by no later than August 2, 2011. As a designated Master Meter, OSU was required to comply with the requirements of section 192.1015. In Oklahoma, these regulations are enforced by the *Oklahoma Corporation Commission* (OCC) and effective June 2021, per notification by OCC, Master Meters in OK are no longer required to use the DIMP process.

NOTE: The Simple Handy Rule based Integrity Management Plan (SHRIMP) is a software platform for developing and managing a DIMP plan.

The pipeline safety code applies to:

- gas utilities (private, public, and municipal),
- operators of housing developments and mobile home parks served by natural gas master meters,
- liquefied petroleum gas (LP-Gas) systems that supply 10 or more customers from a single source; and
- any portion of an LP-Gas system located in a public place, such as a highway.

The determination was made that OSU meets the definition of a Master Meter system and is required to follow the code. The pipeline safety code says that operators of all gas systems must:

- deliver gas safely and reliably to customers,
- provide training and written instruction for personnel,
- establish written procedures to minimize hazards resulting from gas pipeline emergencies, and
- keep records of inspection and testing.

Part 192.619 of CFR Title 49 requires that a *Maximum Allowable Operating Pressure* (MAOP) for the OSU system be established. With the aid of documentation from *Oklahoma Natural Gas Co.* (ONG), the MAOPs (<u>Chapter 14</u>) for seven OSU metering stations have been established as follows:

LOCATION	PSIG	EFFECTIVE APPROVAL DATE
Hall of Fame, West of Monroe Street	35 psig	05/08/1996
1300 Block of North-Western Road	35 psig	05/08/1996
Small Grains Complex	21 psig	05/23/1996
North Side of Power Plant	35 psig	04/13/2020
Beef Cattle Station, north side HWY 51	5.4 psig	
East side of Knoblock - south of McElroy	20 psig	
North side of 4 th St. south of OSU McKnight Performing Arts Center	15 psig	01/26/2018
McElroy and Ramsey	30 psig	02/2023

All gas piping installed after the dates stated in the table shall be based on a pressure test as described in <u>Chapter 13, Leak Repairs - Construction.</u>

It is imperative that OSU routinely meets its responsibilities under the Code because operators who do not comply may be subject to civil penalties, compliance orders, or both. If the hazards warrant, a "Hazardous Facility Order" may be issued that could shut down the OSU gas distribution system.

DEFINITIONS, TERMS, and ABBREVIATIONS

To understand this O&M Plan, one must know the meaning of some commonly used terms in the natural gas and LP- Gas industry. The following terms are commonly used in this arena.

<u>CFR</u> - Code of Federal Regulations include Title 49 a document that contains the actual regulations a natural gas operator must follow. The title number refers to a particular CFR volume.

<u>CATHODIC PROTECTION</u> - A procedure by which underground metallic pipe is protected against corrosion. It is a method for controlling the corrosion or deterioration of steel pipe and connected metallic equipment through the use of electrolysis.

<u>CORROSION</u> - The rusting of a metal pipe. This is caused by an electrochemical reaction that takes place between metallic pipe and its surroundings. As a result, the pipe deteriorates and will eventually leak. Underground corrosion can be retarded with cathodic protection.

CTS – copper tubing size

CUSTOMER METER - A device that measures the volume of gas transferred from an operator to the consumer.

DIMP - Distribution Integrity Management Programs

<u>GAS OPERATOR</u> - A person who engages in the transportation of gas. A gas operator may be a gas utility company, a municipality, or an individual operating a housing project, apartment complex, condominium, or a mobile home park served by a master meter. OSU is considered a gas operator.

IPS – iron pipe size

KEY VALVES - Are the valves needed to shut down the system, or part of the system, in case of an emergency.

<u>LIQUIFIED PETROLEUM GAS (LP-GAS OR LPG)</u> - Gas in a liquid state in the supply tank but vaporized at the tank's outlet then distributed in a gaseous state. LP gas expands when the temperature rises, and it is heavier than air.

MAIN - A gas distribution line that serves as a common source of supply for more than one service line.

<u>MAOP</u> - An abbreviation for maximum allowable operating pressure. This is established by design, past operating history, pressure testing, and pressure ratings.

<u>MASTER METER SYSTEM</u> - A pipeline system for distributing gas within, but not limited to, a definable area, such as a mobile home park, housing project, or apartment complex, where the operator (OSU) purchases metered gas from an outside source for resale through a gas distribution pipeline system. The gas distribution pipeline system supplies the ultimate consumer who either purchases the gas directly through a meter or by other means such as by rent. OSU's system has been determined to be a Master Meter System.

<u>NATURAL GAS</u> - A non-toxic, colorless fuel, about one third lighter than air. Gas burns only when mixed with air in the right proportion and ignited by a spark or flame. Gas in its natural state may not have an odor.

<u>OPERATING and MAINTENANCE PLAN (O&M PLAN)</u> - A plan required by the federal government and created by the system owner that outlines the procedures to be followed in operating and maintaining a safe system.

<u>OVERPRESSURE PROTECTION EQUIPMENT</u> - Equipment installed to prevent pressure in a system. from exceeding the maximum allowed limit for operating the system safely.

<u>PIPELINE</u> - All parts of those physical facilities through which gas moves in transportation. This includes pipes, valves, and other items attached to pipe, meter stations, regulator stations, delivery stations, holders, or fabricated assemblies.

<u>PRESSURE REGULATING/RELIEF STATION</u> - Automatically reduces and controls the gas pressure downstream from a high-pressure source of gas into a system running at a lower pressure. It includes any enclosures, relief devices, and ventilating equipment, and any piping and auxiliary equipment (such as valves, regulators, control instruments, and control lines.)

PSIG - An abbreviation for pounds per square inch gage pressure.

<u>SERVICE LINE</u> - A gas distribution line that transports gas from a common source of supply to a customer's meter, or to the connection to a customer's piping if the piping is farther downstream, or if there is no meter.

SERVICE REGULATOR - A device designed to reduce and limit the gas pressure to the consumer.

<u>SERVICE RISER</u> - The section of a service line which extends out of the ground and is often near the wall of a building. This usually includes a shut-off valve and a regulator.

<u>SHRIMP</u> - Simple Handy Rule based Integrity Management Plan - a software platform for developing and managing a DIMP plan.

<u>SHUT-OFF VALVE</u> - A valve installed to shut off the gas supply to a building. The valve may be located ahead of the service regulator or below ground at the property line or where the service line connects to the main.

SDR - STANDARD DIMENSION RATIO is the ratio of pipe diameter to wall thickness.

COMMONLY ABBREVIATED ORGANIZATIONS

- AGA American Gas Association
- <u>ANSI</u> American National Standards Institute, formerly the United States of America Standards Institute (USASI). All USASI issued standards and current standards issued by ASA have been re-designated as American National Standards (ANS) and continue in effect.
- API American Petroleum Institute
- <u>ASME</u> American Society of Mechanical Engineers
- ASTM American Society for Testing and Materials
- DOT U. S. Department of Transportation
- EHS Environmental Health and Safety OSU
- FM Facilities Management OSU
- ONG Oklahoma Natural Gas Co.
- OSU Oklahoma State University, Stillwater campus
- OQ Operator Qualified
- MSS Manufacturers Standardization Society of the Valve and Fittings Industry
- NACE National Association of Corrosion Engineers
- NFPA National Fire Protection Association
- <u>RSPA</u> Research and Special Programs Administration. This is the federal agency in DOT which is responsible for development and enforcement of the pipeline safety code.

CHAPTER 1 - Methods of Gas Leak Detection

Listed below are eight warning signs of a gas leak with descriptions of leak detection equipment and recommended methods for conducting surface and subsurface leak detection surveys.

WARNING SIGNS OF A LEAK

- <u>Odor</u>. Gas is intentionally odorized so that the average person can perceive it at a concentration well below the explosive range--between ½ to 1% by volume or as local applicable codes dictate. Gas odor is the most common and effective indication of a leak. A report of gas odor should be investigated immediately, and the leak found and repaired. However, the odor of gas may be filtered out as the odorized gas passes through certain types of soil. It may be modified by passing through soil and into a sewage system containing vapors or fumes from other combustibles as well as the sewage odor itself. Therefore, odor is not always totally dependable as an indicator of the presence or absence of gas leaks.
- 2. <u>Vegetation</u>. Vegetation in an area of gas leakage may improve or deteriorate, depending on the soil, the type of vegetation, the environment, the climate, and the volume and duration of the leak. Vegetation surveys of changes in vegetation may indicate slow sub-soil leaks. Vegetation surveys should be supplemented with instrumentation.
- 3. <u>Insects, (flies, roaches, spiders)</u>. Insects migrate to points or areas of leakage due to microbial breakdown of some components of gas. Some insects seem to like the smell of the gas odorant. Be aware of heavy insect activity, particularly near the riser, the gas meter, and regulator.
- 4. <u>Fungus-Like Growth</u>. Such growth in valve boxes, manholes, etc., indicates gas leakage. The color of the growth is generally white or grayish-white and looks like a coating of frost.
- 5. <u>Sound</u>. Listen for leaks. A hissing sound at a bad connection, a fractured pipe, or a corrosion pit hole is the usual indication of a gas leak.
- 6. <u>Unaccounted for Gas</u>. A possible leak is indicated when an off-peak reading of a master meter, with a known average seasonal utilization rate, shows an unaccountably high usage rate. Periodic off-peak checks (preferably the summer months from midnight to three or four o'clock in the morning) can be averaged to provide data for comparison in future checks. Gas leaks served by a master meter system can be detected by comparing the total consumption registered on the customer meters with that registered on the master meter. If the master meter reading is greater than that recorded by adding all the unit meter readings, then a leak probably exists in the distribution system. This condition may also indicate a gas theft problem or a malfunctioning meter problem.
- 7. <u>Soap Bubbles</u>. A soap solution can pinpoint the location of a leak on an exposed pipe, on the riser, or the meter. The solution is sprayed onto the area in question and the location of bubbling indicates leakage.
- 8. <u>Leak Detection Instruments</u>. Gas leak indicators are sophisticated instruments that require regular care, maintenance, and calibration, and should be used only by trained personnel. OSU uses qualified outside vendors who are familiar with this equipment to perform annual leak surveys as noted in Appendix C of this document.

CHAPTER 2 - Reports and Plans Required by the Federal Government

The federal government requires every gas operator to report any incident and to follow and maintain records according to established Operating and Maintenance (O&M) and Emergency plans. This section provides an overview of these plans.

INCIDENT REPORT

See Emergency Plan

OPERATING & MAINTENANCE (O&M) PLAN for OSU

An O&M plan is required of all gas operators by the Pipeline and Hazardous Materials Safety Administration (PHMSA) 49 CFR 192.603. The O&M plan contains the steps that must be followed to accomplish the required operational and maintenance procedures.

DISTRIBUTION INTEGRITY MANAGEMENT PLAN

On December 4, 2009, PHMSA published the final DIMP rule. The rule required each operator of a natural gas utility, master meter system or propane pipeline system to prepare and follow a written DIMP plan by no later than August 2, 2011. This rule required each operator to demonstrate:

- Knowledge of system infrastructure
- Identify threats.
- Evaluate and prioritize risk.
- Identify and implement measures to mitigate risks.
- Measure performance, monitor results, and evaluate effectiveness.
- Periodic Evaluation and Improvement
- Report results

Five years of data was entered into a database utilizing the SHRIMP tool, developed by the APGA Security and Integrity Foundation. Based on OSU's historical data, we identified no threats or risks to prioritize. This was an indication that the steps we defined in our O&M Manual were adequate and sufficient to maintain the integrity of and mitigate the potential for accidents in our jurisdictional gas system. OSU's intent is to continue to operate according to this manual and continue to evaluate any potential threats as additional information is compiled on a regular basis. Consistent with the exclusions in 49 CFR §191.9 (incident reports) and §191.11 (annual reports), operators of master meter and small LPG distribution systems need not report performance measures. <u>Master meter systems in OK are no longer required to utilize the DIMP tool, as per OCC effective Summer 2021.</u>

CHAPTER 3 – Materials Qualified for Use in Gas Systems

The federal regulations contained in 49 CFR Part 192 list many varied materials qualified for gas service. The materials and specifications listed in this manual are those that are most commonly used in gas distribution systems installed in the early 1980's. Not all qualified materials or specifications listed in Part 192 are included in this chapter.

When purchasing material used in a gas system, it is extremely important to check the *marking* of the material. The marking on the material will help identify whether the material is qualified for gas service. An operator must select materials that are compatible with each other. This chapter covers the most common specifications and standards used by manufacturers for pipes, valves, flanges, regulators, and other equipment commonly used in gas distribution systems.

<u>PIPE</u>

Only steel and plastic pipe specifications are included in this chapter. (For other qualified pipe specs see Appendix A of 49 CFR - Part 192.)

STEEL PIPE

API 5L - Steel Pipe ASTM A53 - Steel Pipe ASTM A381 - Steel Pipe ASTM Specification A671 - Steel Pipe ASTM D2513 - Thermoplastic Pipe and Tubing

Nominal Pipe Size	Outside Diameter	Standard (Schedule 40) Wall Thickness	Minimum Wall Thickness after Threading
1/8	0.405	0.068	0.065
1/4	0.540	0.088	0.065
3/8	0.675	0.091	0.065
1/2	0.084	0.109	0.065
3/4	1.050	0.113	0.065
1	1.315	0.133	0.065
1 1⁄4	1.660	0.140	0.065
1 1/2	1.900	0.145	0.065
2	2.375	0.154	0.075
3	3.500	0.216	0.098
3 1/2	4.000	0.226	0.108
4	4.500	0.237	0.116
5	5.563	0.258	0.125
6	6.625	0.280	0.156
8	8.625	0.322	0.172
10	10.750	0.365	0.188
12	12.750	0.406	0.203

Guide for selecting the proper nominal wall thickness for <u>steel pipes</u> used in a gas distribution system. Measurement is in INCHES.

All new steel pipes manufactured under the above specifications with the above wall thickness have design pressure up to at least 152 psig. Operators are cautioned that the actual MAOP of a new or replacement pipe in a gas system is dependent upon the pressure test performed on the pipeline system before it is put in service. It is recommended that threaded pipes not be installed underground.

POLYETHYLENE (PE) PLASTIC PIPE

When purchasing <u>polyethylene (PE) plastic pipe</u>, it is required that the pipe be marked <u>ASTM D2513</u>. Plastic pipe with this marking is suitable for gas service. <u>Fiberglass epoxy plastic pipe</u> marked <u>ASTM D2517</u> is also qualified for gas service.

At no time should the loading of the pipe cause the pipe section to lose its round shape. Plastic pipes and tubing should be stored and protected from damage by crushing, piercing, or extended exposure to direct sunlight.

As a rule of thumb, never store plastic pipe outdoors for more than 6-months. It should be placed inside or covered to protect it from exposure to direct sunlight. It is a good idea to obtain the manufacturer's recommendation as to how long the pipe can be exposed to sunlight before it loses some of its physical strength. In recent years, the vast majority of natural gas companies have been installing ASTM D2513 PE pipe. Benefits of PE pipe are flexibility, good joining characteristics, durability, ease of installation, and cost. The PE designations most often used are PE 2306, PE 3306, PE 3406, and PE 3408.

Most PE pipe manufacturers subscribe to the *Standard Dimension Ratio* (SDR) method of rating pressure piping. The SDR is the ratio of pipe diameter to wall thickness. An SDR 11 means the outside diameter (OD) of the pipe is eleven times the thickness of the wall.

For high SDR ratios the pipe wall is thin in comparison to the pipe OD. Given two pipes of the same OD, the pipe with the thicker wall will be stronger than the one with the thinner wall. High SDRs have low pressure ratings; low SDRs have high pressure ratings because of the relative wall thickness.

This table below is intended to be a guideline. Personnel should check the manufacturer's specific pressure rating for each specific pipe.

HYDRO	STATIC D	DESIGN E	BASIS (HE) DB)						D2513
PSI	6.0	7.3	9.0	11	13.5	17	21	26	32.5	Letter Code
1600	200	160	125	100	80	64	50	40	32	G
1250	160	125	100	80	64	50	40	32	25	F
1000	125	100	80	64	50	40	32	25	20	E
800	100	80	64	50	40	32	25	20	16	D
630	80	64	50	40	32	25	20	16	12.5	С
500	64	50	40	32	25	20	16	12.5	10	В
400	50	40	32	25	20	16	12.5	10	8	Α

PRESSURE RATING for PE PIPE (2406 and 3406) LISTED by ASTM D2513 STANDARD DIMENSION RATIO (SDR)

Plastic pipe is purchased according to the iron pipe size (IPS) or the copper tubing size (CTS).

Be aware that the actual MAOP of new extension or replacement pipe in a gas system is dependent upon design pressure of the pipe and components in the system, and the pressure test performed by the operator or their contractor on the piping system.

Before placing in service, OSU must test each disconnected service line in the same manner as a new service line (49 CFR 192.725). The pressure testing requirements for plastic and metallic service lines are listed under "Plastic Pipe Installation - Rule 9" and "Metallic Pipe Installation" found in <u>Chapter 16</u>.

PE pipe may be joined by either the heat fusion method (butt, socket, or electrofusion) or by a mechanical coupling. Personnel performing the joining procedure must be <u>properly qualified</u> for heat fusion, for each pipe material, or combination of materials being joined.

PE pipe that is not encased must have a minimum wall thickness of 0.090 inches. However, pipe with an OD of 0.875 (¾" nominal size) or less may have a minimum wall thickness of 0.062. Acrylonitrile-butadiene-styrene (ABS), Cellulose acetate butyrate (CAB), Polybutylene (PB), and Poly vinyl chloride (PVC) are also types of plastic pipe qualified for natural - NOT LP - gas service <u>if the pipe has the ASTM D2513 marking on it</u>. However, most natural gas companies no longer install these types of plastic pipes in their gas systems because they believe that PE pipe has superior characteristics.

VALVES

Each valve must meet the minimum requirements or the equivalent API 6D. <u>A valve may not be used under</u> operating conditions that exceed the applicable pressure-temperature rating contained in the standard. The valve will be stamped with either the class (ANSI) or the maximum working pressure rating (PSIG). Never operate valves at pressures that exceed their rating.

The class of ANSI ratings on steel valves are ratings which specify the maximum working pressure for flangedend and weld-end gate, plug, ball, and check valves.

Class Rating (ANSI) Maximum Working Pressure Rating (PSIG)

				<u> </u>	0.07		
ANSI	150	300	400	600	900	1500	2500
PSIG	275	720	960	1440	2160	3600	6000
TI					r 00		

The maximum working pressure ratings are applicable at temperatures from -20°F > 100°F.

<u>Metal valves</u> will often be stamped with the symbols WOG. This means that they are suitable for service for water, oil, or gas. Sometimes just the letter G (for gas) appears.

The manufacturer's name or trademark will also be included on a valve. OSU installation personnel should maintain manufacturers' manuals that include installation, operation, and maintenance procedures for each different type of valve in the gas system. These manuals and procedures are to be always maintained and accessible to system maintenance personnel.

There are <u>plastic valves</u> that are suitable for gas service. Plastic valves purchased for gas service should comply with industry standard ANSI B16.40. *Manually Operated Thermoplastic Valves in Gas Distribution Systems*. The valves must be compatible with the plastic pipe used in gas systems. When buying plastic valves, record specifications and information on suppliers who are knowledgeable in the gas piping field.

FLANGES and FLANGE ACCESSORIES

Each flange or flange accessory (other than cast iron) must meet the minimum requirements of ANSI B16.5, MSS SP-44, or the equivalent. For cast iron, refer to 49 CFR 192.147 (c). For plastic fittings made of PVC or ABS plastic, refer to 49 CFR 192.91.

Installation personnel should verify that metal flanges purchased for the OSU system meet the above requirements. This can be done by checking the markings on the flange. The markings are similar to those on the valves.

REGULATORS and OVER PRESSURE PROTECTION EQUIPMENT

There are many different manufacturer models of gas regulators and over pressure equipment (relief valves) available for gas systems. Regulators and over-pressure protection equipment must be properly sized so that over pressure or low-pressure conditions do not occur on the gas system. Manufacturers of gas regulators and relief valves have manuals which contain formulas and charts for each of their specific models or types of equipment. These formulas and charts are necessary to size regulators and relief valves properly.

Obtain manufacturer operation and maintenance instructions for each individual type of regulator and relief valve in the OSU system. Normally, the manufacturer publishes a manual containing these instructions. These manuals are to always be accessible to system maintenance personnel.

CHAPTER 4 – Personnel Instructions

The following instructions cover operating and maintenance procedures which <u>must be followed</u> during normal operations and while making repairs (49 CFR 192.605(c)).

Normal Operations

- 1. Personnel shall observe caution when utilizing power equipment in and around aboveground gas distribution devices such as meters and regulators.
- 2. Welding and heat sources shall not be used adjacent to above ground gas distribution devices unless approved by the OSU EHS Director, and appropriate permitting is obtained.
- 3. Prior to working around natural gas devices, personnel shall make certain that there is adequate ventilation, and no leaks. Operator Qualified (OQ) OSU personnel shall check for gas and O₂ content of work site air and confirm safety of atmosphere. Installation personnel shall check for leaks. For added safety, fire extinguisher(s) shall be readily available during all work on gas lines.
- 4. Lock-out/tag-out procedures shall be used on all gas fired equipment and/or isolation valves when maintenance work being performed could result in an unintentional release of gas.
- 5. Any personnel who smell gas or observes problems with any gas distribution device or equipment shall report it immediately to their supervisor.
- 6. After hours problems shall be reported according to the NG OUTAGE COMMUNICATION TREE.
- 7. Any planned work in and around gas pipelines or devices where OSU owned ground needs to be opened requires an OSU Excavation Permit and confirmation that all relevant OSU and outside agencies have marked all known underground lines in the area. In addition, if work being performed is within 5-ft of a NG line, at least one approved OSU personnel must be available to witness work being performed. Locate requests begin by calling Oklahoma One-Call (OKIE) at 811. OKIE notifications are received by Energy Services personnel who then inform FM Work Control to process an Excavation Permit.

While making repairs

1. Any repair work on the gas distribution system that could result in the unintentional release of gas will require lock-out and tag-out of the line at the meter or nearest upstream valve.

- 2. All OSHA Safety Requirements shall be met when opening the ground to work on pipelines.
- 3. Only material qualified for use in gas systems may be used for repair purposes. Materials must meet requirements noted in <u>Chapter 3</u> of this manual.
- 4. When a line is opened there must be no sources of ignition operating in the area. OQ OSU personnel shall monitor atmospheric conditions.
- 5. If any unsafe conditions develop, personnel shall vacate the area immediately and contact the appropriate supervisor or emergency response personnel as dictated by the situation.
- 6. Work areas shall be responsibly safeguarded in order to keep students, staff, faculty, and all others at a safe distance from the work being performed.
- 7. All repairs are pressure tested to ascertain if they will hold up under operating pressures.
- 8. No person shall work on any part of the gas pipeline system unless such person is deemed qualified by OSU ES Utilities Distribution training records.

CHAPTER 5 – Line Marking Process

LINE MARKERS

- 1. All PE gas pipes installed underground shall be buried with a metal tracer wire to facilitate location when necessary.
- 2. Wire shall be No. 12 AWG copper clad steel wire or Copperhead brand or approved equal rated for direct burial application.
- 3. The insulation shall be yellow.
- 4. Wire shall be directly above and within 2" to 3" of the line but shall not contact the line at any point.
- 5. All gas pipes, regardless of material, are to be buried with a yellow marker tape approximately 12" above the line.

CHAPTER 6 – Patrolling and Continuing Surveillance

OSU patrols mains located in places or on structures where anticipated physical movement or external loading (weight, traffic) could cause failure or leakage (49 CFR 192.721). These places or structures include areas susceptible to earth subsidence (cave ins), or areas of construction activity. Patrolling can be done by walking along the pipeline and observing factors affecting safe operation. Patrolling of these mains is done annually and recorded on the <u>Surveillance/Patrolling Form</u>.

Patrolling also includes the annual inspection of regulators. Inspection assures proper operation of regulators, checks installation, and assures that vent screens are in place with no obstructions. Inspections are documented on the <u>Surveillance/Patrolling Form</u>.

Continuing surveillance is an ongoing process, and all personnel are instructed to constantly be vigilant for abnormal situations. If a threat is identified, OSU personnel must take appropriate action and ensure that necessary documentation is completed.

CHAPTER 7 – Gas Leak Surveys

A leakage survey of OSU's NG distribution system must be made as frequently as necessary, at intervals not exceeding 15-months, and at least once each calendar year (49 CFR 192.723). The survey shall be conducted on all exterior natural gas piping under OSU's authority.

Any leak that is found should be classified as soon as it is located. When a leak is discovered, it must be investigated to determine if a hazard exists. If a leak is deemed hazardous it must be repaired immediately, and OSU must protect life and property until conditions related to the leak are no longer hazardous. All leak repairs – whether hazardous or not, are documented through the FM work order system.

NG system surveys are conducted annually during the growing season and may be conducted by meter readers or other maintenance personnel. All leaks discovered must be recorded. Document survey results on the <u>appropriate form</u>, whether or not leaks are found.

Specifications for the OSU STW NG Survey.

1. SURVEY SCHEDULE

The annual gas leak survey is performed by a qualified NG piping system leak testing business and coordinated by ES Utilities Engineering. The survey is scheduled to begin mid-June each year with a six-week allowed performance time ending July 31.

2. PROJECT DELIVERABLES

- 1. Daily Report A summary of the day's survey result shall be provided to the accompanying OSU ES staff at the end of each day.
- 2. Annual Report Due at completion of annual survey delivered to the ES Utilities Engineering Manager Includes results & findings from leak survey and odorant test.
 - a. Field Report
 - i. A copy of the completed field report.
 - b. Final Bound Report
 - i. A bound final report for the NG system campus manager for their records.
 - c. A final report in electronic format (on a thumb drive)

CHAPTER 8 – Shutdown and Abandonment of Facilities

SHUTDOWN

When it is necessary to shut down any area in the OSU natural gas system, personnel should go to the first available zone valve. If the area is looped, all lines serving the loop must be valved off. Steps are to be taken to minimize the number of affected buildings. Follow established tag-out procedures.

Once the need for the shutdown is past, reopen valves. When the system is back on-line, blow off any air that has accumulated in the pipeline and perform a sniff test.

ABANDONMENT

When an OSU gas main or service line is abandoned, it must be physically disconnected from the piping system and the open ends effectively sealed. In addition, personnel must determine the necessity of purging the line. All pipe 4" and larger shall be purged as follows.

a) When a pipeline or main full of air is placed in service, the air in it can be safely displaced with gas provided that a moderately rapid and continuous flow of gas is introduced at one end of the line and the

air is vented out the other end. The gas flow should be continued without interruption until the vented gas is free from the air. The vent should then be closed.

- b) In cases where gas in a pipeline or main is to be displaced with air and the rate at which air can be supplied to the line is too slow to feasibly perform a procedure similar to, but the reverse of (a), then a slug of inert gas should be introduced to prevent the formation of an explosive mixture at the interface between gas and air. Nitrogen or carbon dioxide can be used for this purpose.
- c) If a pipeline or main containing gas is to be removed, the operation may be carried out in accordance with (b), or the line may first be disconnected from all sources of gas and then thoroughly purged with air, water or with inert gas before any further cutting or welding is done.

In cases where the main and all the service lines connected to it are abandoned, the service line(s) must be capped at the customer's end. The abandoned main must be sealed at both ends.

Records must be kept on all abandoned facilities. This includes location, date, and method of discontinuing service (abandoning the facility). All information on any abandoned lines is reported as soon as possible to FM Energy Services, Utilities Distribution, and incorporated into the ES record of abandoned gas lines available in GIS.

When service to an OSU facility is temporarily or permanently discontinued, one of the following must be done:

- a) The valve must be closed to prevent the flow of gas to the customer, and the valve must be <u>secured with</u> <u>a lock or some other device</u> to prevent opening of the valve by unauthorized people.
- b) <u>A mechanical device or fitting</u> that will prevent the flow of gas must be <u>installed</u> in the service line or in the meter assembly.
- c) The customer's piping must be <u>physically disconnected</u> from the gas supply and the <u>open ends sealed</u> (49 CFR 192.727).

For pipeline shutdowns, go to the first available workable zone valve to shut down the problem area. Isolate so as to minimize the number of buildings affected, making sure the entire loop (if applicable) is isolated. Use tag-outs on all valves used. After the shutdown work is completed, open all valves in the reverse order in which they were closed. Blow off any air that has accumulated in the line and do an odorant sniff test.

CHAPTER 9 – Preventing Accidental Ignition of Gas

Gas alone is not explosive but when it is mixed with air, it can ignite or explode with tremendous force. OSU personnel should take every precaution to prevent unintentional ignition of gas.

When venting gas into air, a fire extinguisher must be available (49 CFR 192.751), and all heat or ignition sources kept far away from the source of the venting.

CHAPTER 10 – Key Valves Maintenance

The key valves must be checked and serviced at intervals not exceeding 15-months, but at least once each calendar year. Records of this inspection must be maintained (49 CFR 192.747). Key valves are indicated on the Campus Jurisdictional Gas Map available in GIS.

Inspect and Service Valve

<u>NOTE</u>: Each distribution line valve that might be required during an emergency must be inspected and partially operated at intervals <u>NOT</u> exceeding 15-months, but at least once each calendar year. During valve inspection, any abnormal condition of valve or pipeline or existence of leakage must be documented and reported.

ABOVE GROUND INSPECTION:

Visually INSPECT for external damage.

- 1. VERIFY nameplate is visible and legible.
- 2. INSPECT for leaks:
 - a. Flange
 - b. Bonnet joints
 - c. Packing gland
- 3. INSPECT for:
 - a. General condition
 - b. Lubrication
 - c. Freedom of movement
- 4. INSPECT for abnormal operating condition of valve or pipeline:
 - d. Unintended pipe movement
 - e. Corrosion
 - f. Material defect
 - g. Physical damage
- 5. IF ANY abnormal conditions are observed, NOTIFY the Supervisor

IF a leak is found, THEN:

- 1. IF practical, ATTEMPT to isolate or stop the leak and notify Supervisor.
- 2. IF a serious leak is detected and presents a hazard to persons, follow <u>NG Emergency Operations Plan</u> procedures.

RECORD all results in AiM as directed.

SERVICING:

- 1. PERFORM servicing per manufacturer's specification.
 - a. For gate and ball valves:
 - i. IF possible, WHILE valve is in CLOSED position, BLOW DOWN valve body.
- 2. INSPECT for block and bleed capabilities.
 - a. IF body is capable of being blown down, but does not depressurize, THEN.
 - i. Indication is leakage by seats caused by valve not being fully closed.
 - ii. Indication is probable damage to seats or seating surfaces.

NOTIFY Supervisor and/or other appropriate personnel.

NOTE: Most ball and gate valves do not require lubrication except when needed to help seal damaged seats, gates, or balls.

LUBRICATION: CHECK manufacturer's specifications for lubrication.

- 1. LUBRICATE plug valve bodies with appropriate lubricant.
 - a. Hand wheel grease fittings
 - b. Stem
 - c. Packing gland studs
 - d. Nuts
- 2. INSPECT packing glands on valve stems for leakage AND,
- 3. ADJUST or ADD packing, if required, to stop leaking.

NOTE: Operate valves fully, when possible, otherwise, partial operation is acceptable. When operating the valve, take care to prevent disrupting service or over pressurizing the system

EVALUATE consequences of operating valve AND TAKE necessary precautions to minimize impact.

- 1. IF bypass piping and valves are present
 - a. Unlock and open bypass before operating the main line valve.
- 2. STROKE main line valve full travel, if possible, AND ensure valve operates freely with NO binding.
- 3. RETURN main line valve to previous position AND shut and lock bypass valve.
 - a. If bypass piping and valves are <u>not present</u>, FOLLOW guidelines in NOTE box above.

INSPECTION: Underground poly valves:

- 1. Check area for AOC and note on inspection form.
- 2. Check valve lid for paint and ensure lid is marked GAS.
- 3. Remove lid from box and check riser for the presence of tracer wire. Remove any trash or dirt in the riser.
- 4. Place wrench on valve and turn 1/8 of a turn in the shut direction.
- 5. Re-open valve. Perform sniff test at riser opening to detect possible leakage.
- 6. Replace valve box lid and re-paint if needed.

RECORD Inspection results in AiM as directed.

CHAPTER 11 – Measuring and Odorization of Gas

OSU must verify that a person with a normal sense of smell can detect gas in air at <u>one-fifth the lower explosive</u> <u>limit</u>, which is approximately 1% gas-in-air.

OSU complies with this requirement by including odorometer testing as part of its annual comprehensive leak survey.

<u>Note</u>: Periodic *sniff tests* can be a guide in determining odorization levels even though they do not replace the need to maintain odorant usage records or perform odorometer tests. OSU maintenance personnel shall smell the gas at an open valve or gas oven burner during meter change-outs or other maintenance work. Records of sniff tests shall be maintained and, when possible, should be run at the ends of the system.

CHAPTER 12 – Corrosion Control

The OSU natural gas distribution system does not have cathodic protection. Records are insufficient to determine whether the remaining metallic pipe in the system was installed before or after August 1, 1971. OSU does not believe that initiating a corrosion control program at this time would be of benefit to the University. This view is based on the following:

- Since 1985, OSU has pursued an aggressive annual natural gas system leak survey program and plans to continue this annual survey, not only to conform with federal and state mandates, but also be initiative-taking in its pursuit of safety in the gas system.
- The decision was made in the late 1980's to embark on a program for the replacement of underground metallic natural gas distribution lines with polyethylene material. Most known underground lines on OSU's Stillwater campus operating at the MAOP have been replaced in this program. It is the view of OSU that replacement of metallic lines with plastic is the best way of combating the corrosion problem that afflicts metallic lines. As underground metallic lines operating at the MAOP are discovered they shall be scheduled for replacement with polyethylene.

Above ground piping and below ground piping must be electrically separated using anodeless risers. Above ground piping is protected by use of coatings (painting) of the pipe. This places a barrier between the pipe and the outside elements. This protection must be suitable to prevent corrosion caused by moisture, i.e., rain, fog, sprinklers, coolers, or any other source of moisture. All metallic above ground facilities must be evaluated for atmospheric corrosion at least once every three years and results documented in AiM as directed.

CHAPTER 13 – Leak Repairs and Construction

Repair, construction, and safety are based upon good common sense and sound engineering concepts. This chapter is designed to increase the safety of OSU's gas system by helping meet the construction and repair standards set by the pipeline safety code.

The manufacturers of pipes, valves, fittings, and other gas system components must design and test them to prescribed industry specifications. The specifications are incorporated into 49 CFR Part 192. Those meeting the requirements are qualified for gas service and marked with the *approved markings*. In addition, manufacturers usually develop procedures for joining their products and joining other materials to their products. This chapter outlines construction, pipe handling, and pressure testing requirements that should be followed when installing a gas system. Plastic pipe fusion instructions and steel pipe welding and qualification procedures are

included in <u>Chapter 16</u>. These instructions and procedures explain the steps necessary to qualify a person to make pipe joints/welds for either plastic or steel pipe. They give directions for finding qualified people to do the construction and repair work on the system. <u>If a gas contractor is used to work on the system, it is OSU's</u> responsibility to see that the contractor follows all requirements. However, it shall be OSU's policy that OSU trades and utilities personnel will, whenever possible, join all jurisdictional piping on projects involving outside contractors. In the event OSU cannot perform this service, the contractor will be required to follow all procedures and present all necessary documentation as mandated by 49 CFR Part 192 and outlined in OSU's Engineering Guidelines/NG Construction Standard.

PLANNING AHEAD

Before making modification or repair of a piping system, comprehensive plans should be made. It is essential that OSU installation personnel know the type of material and all the parts that make up the present gas piping system. The piping system consists of pipe, valves, fittings, regulators, relief devices, and meters. By knowing the type of material in the system, the proper fittings can be selected.

EXCAVATION

Before digging for gas line installation, repair, or replacement, <u>the pipe network and other underground utility lines</u> <u>must be located</u> on the property. Call OKIE to notify others who may have underground lines in the excavation area. Lines may be located by one or all of the following ways:

- Locate all underground utility lines on *as-built* or *corrected-for-construction* drawings. Maps or drawings of the location of the underground gas lines are particularly important. They can provide information to other utilities that must dig to repair or replace their utility lines. Any changes made in the system must be reported to FM Utilities Distribution so the drawings can be updated.
- Locate underground metallic utility lines with pipe locating instruments. Plastic pipe which was installed with an electrically conductive wire can also be located by this method. Pipe locating instruments are to be used in accordance with manufacturer's operating procedure; OSU personnel primarily use the Radio detection RD 8100 (procedure for this unit located in <u>Chapter 17</u> of this manual).
- Locate or verify locations of other underground utility lines serving the area. The line marking process is described in <u>Chapter 5</u>.

Be aware that service lines and mains built prior to the enactment of minimum depth requirements may be very shallow. Therefore, digging to expose gas lines for repair or replacement purposes should be carried out with hand tools (preferably made of brass or other non-sparking material) until the gas lines are located. Afterwards, power tools may be used.

When working on a leaking pipe, a stand-by worker should be ready to assist their partner in escaping from the hole in the event of an emergency. A fire extinguisher must be available during all such repairs.

PIPE INSTALLATION, REPAIR, AND REPLACEMENT: GENERAL COMMENTS

Gas service lines and mains are to be installed with a minimum of 24" of earth cover. Purging of new lines shall be accomplished in accordance with Abandonment of Facilities in <u>Chapter 8</u>.

Underground structures may prevent the installation of gas services or mains at minimum depths. The pipeline safety regulations allow a shallower depth of cover if adequate protection is provided (i.e., sufficient to withstand the anticipated external loads - e.g., heavier pipe, casing, concrete, etc.). In such cases, it is recommended that the gas line's location be marked above ground. The area should be inspected <u>frequently</u> to ensure that the ground cover is intact and has not eroded (49 CFR 192.327 & 192.361).

OSU must document all leak repair data. Repairs should be done through the FM AiM work order system. Records must include leak reports received from customers.

METALLIC PIPE INSTALLATION

All the conditions listed below must be met when metallic pipe is installed. Although OSU intends to install PE pipe exclusively in the future, this material is included for reference purposes.

- 1. Make each joint in accordance with written procedures that have been proven by test or experience to produce strong gas tight joints.
- 2. Obtain and follow the manufacturer's recommendations for each specific fitting used.
- 3. Handle pipe properly without damaging the outside coating. Any gouges or scratches should be covered with an appropriate coating. If coating damage is not corrected, accelerated corrosion can occur in that area.
- 4. Coat or wrap steel pipe at all welded and mechanical joints before backfilling.
- 5. Pressure test new pipe for leaks before backfilling as follows:

Mains operated at <1 psig	Test to at least 10 psig
Mains operated at 1 psig or > but < 10 psig	Test to at least 90 psig
Service lines operated at 1 psig but not more than 40 psig	Test at not less than 50 psig

- 6. Support the pipe along its length with proper backfill.
- 7. Make certain that backfill material does not contain stones, cinders, bottles, or cans that may damage or scratch pipe coating.
- 8. Cathodically protect steel pipes.
- 9. Electrically insulate dissimilar metals.
- 10. Make certain that compression type fittings that are intended to be electrically conductive have armored gaskets. Bond over insulating fittings to maintain electrical continuity for cathodic protection and for locating steel pipe.

If personnel must weld steel in the pipeline, they should review the pipeline safety requirements covered in Subpart E of 49 CFR Part 192, provide qualified welders to perform the welding, and follow the qualified welding procedures contained in <u>Chapter 16</u>. With the current material available for gas service (repair fittings, clamps, sleeves, tees, etc.), there should be little need to do much welding on a small gas distribution system for operation and maintenance purposes. The important things to remember are that welding <u>must be performed in accordance with established written welding procedures</u> that have been qualified and tested to produce sound ductile welds, and welding <u>must be performed by welders who are qualified</u> for the welding procedure to be used. Both the procedures and the personnel must be qualified for the type of welding performed.

OSU has adopted the qualified welding procedures for metallic pipes which is based on Section IX of the ASME Boiler and Pressure Vessel Code. OSU will qualify its on-staff welders to weld on the OSU steel gas system per provisions of 49 CFR 192.227 (b), Appendix C - Qualification of Welders for Low Stress Level Pipe and using the specifications of the procedure as contained in <u>Chapter 16</u> of this manual.

PLASTIC PIPE INSTALLATION

Plastic pipes are now commonly used for distribution mains and services by the gas industry. The most common type of plastic pipe presently installed is polyethylene (PE). <u>PE plastic pipe is the only acceptable plastic for LP-Gas piping and is recommended as the most suitable plastic pipe for natural gas piping</u>. PE plastic pipe is manufactured according to ASTM D2513 and is marked with that number.

Plastic pipes may be buried directly in the ground. It may also be used to replace a deteriorated buried metal pipe. In these cases, a slightly smaller plastic pipe is generally inserted into the existing metal pipe.

Each plastic pipe joint must be made in accordance with written procedures that have been proven by test or experience to produce strong gas tight joints. Plastic pipe joining procedures must be qualified according to the requirements contained in 49 CFR 192.283. The personnel who make the joints must meet the requirements contained in 49 CFR 192.285. OSU need not run the tests described in 49 CFR 192.283 themselves because most pipe and fitting manufacturers develop and qualify joining procedures for each specific product. Do not purchase the product if it cannot be certified that the manufacturer or supplier of the pipe or fitting has the joining procedures which meet the requirements of 49 CFR 192.283.

Manufacturers of both pipe and fittings have installation manuals, which describe the specific joining procedures required to make a strong, gas-tight joint. Manufacturers' procedures for each of the pipeline components that are used in the system must be easily accessible for OSU installation personnel.

49 CFR 192.273 requires that <u>each joint</u> be inspected before the gas line is put into service. Per 49 CFR 192.287, those who inspect these joints must be qualified to do so. OSU considers a person as qualified if they are also qualified to make such joints per 49 CFR 192.285. When a joint is inspected, <u>documentation of the inspection is required and must be kept on file.</u>

According to the safety standards (49 CFR 192.285), a person making joints must be qualified. 49 CFR 192.285 provides requirements for qualifying persons to make joints:

- 1. No person may make a plastic pipe joint unless that person has been qualified under the applicable joining procedure by:
 - a. Appropriate training or experience in the use of the procedure; and
 - b. Making a specimen joint from pipe sections joined according to the procedure that passes the inspection and test set forth in paragraph (b) of this section.
- 2. The specimen joint must be:
 - a. Visually examined during and after assembly or joining and found to have the same appearance as a joint or photographs of a joint that is acceptable under the procedure; and,
 - b. In the case of a heat fusion, solvent cement, or adhesive joint:
 - i. Tested under any one of the test methods listed under 49 CFR 192.283(a) applicable to the type of joint and material being tested:
 - ii. Examined by ultrasonic inspection and found not to contain flaws that would cause failure; or
 - iii. Cut into at least 3-longitudinal straps, each of which is:
 - 1. Visually examined and found not to contain voids or discontinuities on the cut surfaces of the joint area; and
 - 2. Deformed by bending, torque, or impact, and if failure occurs, it must be initiated in the joint area.
- 3. A person must be re-qualified every twelve months by the method indicated in (b) (ii) and (iii) above. <u>Test</u> strips and re-qualification documentation must be maintained on file.

The general rules to follow when installing plastic pipe are listed below:

 Rule 1:
 Install plastic pipe manufactured under the ASTM D2513 specification. The pipe must have ASTM

 D2513 marked on it.

- Rule 2: Make each joint in accordance with written procedures that have been <u>proven by test or experience</u> to produce strong tight joints. The manufacturer of the pipe or fitting should supply the procedures for his specific product in the manufacturer's manual. When installing the pipe, make certain that these procedures are followed (49 CFR 192.283). All joints must be made by a person qualified under 49 CFR 192.285.
- Rule 3: Install properly designed valves in a manner which will protect the plastic material. Protect the pipe from excessive torsion (twisting) or shearing (cutting) loads when the valve is operated. Protect from any secondary stresses which might be induced through the valve or its enclosure.
- Rule 4: Prevent pullout and joint separation. Plastic pipe must be installed in such a manner that expansion and contraction of the pipe will not cause pullout or separation of the joint. Operators unfamiliar with plastic pipes should have a qualified person perform all these procedures.
- Rule 5: When inserting plastic pipe in a metal pipe, make a sufficient allowance for thermal expansion and contraction. Make an allowance at lateral and end connections on inserted plastic pipes, particularly those over 50' in length. End connections must be designed to prevent pullout caused by thermal contraction. It is desirable that fittings used should be able to restrain a force equal to or greater than the strength of the pipe. If not, the pipe should be restrained by anchoring, bracing, offset connection, or straps across the fitting. To minimize the stresses caused by thermal contraction, pipes inserted in the summer should be allowed to cool to ground temperature before tie-ins are made. Inserted pipes, especially those pulled in, should be relaxed, mechanically compressed, or cooled to avoid initial tensile stress.
- Rule 6: Repair or replace imperfections or damage before placing the pipe in service.
- Rule 7: Install all plastic mains below ground level (buried). Where the pipe is installed in a vault or other below-grade enclosure, it must be completely encased in gas-tight metal pipe with fittings that are protected from corrosion. (For service line, see Rule 8.) The plastic pipe installation must minimize shear and other stresses. Thermoplastic (PE) pipes for direct burial must have a minimum wall thickness of 0.090 inch. (Exception: pipe with an outside diameter of 0.875" (7/8") or less may have a minimum wall thickness of 0.062".) A plastic main that is not encased must have an electrically conductive wire or other means of locating the pipe while it is underground.
- Rule 8: Install all plastic service lines below ground. A portion of the plastic service line may terminate above ground if it is protected against deterioration and external damage by a casing. Plastic must not be used to support external loads. There are many different manufacturers of anodeless risers. The primary advantage of an anodeless riser is that it does not have to be cathodically protected because the outside steel casing is not the gas carrier. The plastic inside the steel casing is the gas carrier. If anodeless risers are purchased, make sure they meet all DOT requirements. If steel risers are installed connected to plastic pipe by a transition fitting, make sure the steel riser is coated and cathodically protected.
- Rule 9: Test installed plastic pipe at least at a level 150% of the maximum operating pressure or 50 psig, whichever is greater. However, the test pressure may not be more than three times the design pressure of the pipe. When a pipe is received from the vendor, the joints or spools shall be subjected to the test pressures noted above. If the pipe passes the test, it shall be identified by markings as to

date and pressure of test, documented. As pipe is used, it is charged to a work order which indicates the location of use. All testing is to be documented.

- Rule 10: Take special care to ensure that plastic pipe is continually supported along its entire length by properly tamped and compacted soil.
- Rule 11: If plastic pipe is laid where there has been digging and backfilling below the pipe, reinforce the pipe. To prevent any shear or other stress concentrations, use external stiffeners at connections to main, valves, meter risers, and other places where compression fittings might be used.
- Rule 12: In the laying of plastic pipe, ensure adequate slack (snaking) in the pipe to prevent pullout due to thermal contraction.
- Rule 13: Lay plastic pipe and backfill with material that does not contain any large or sharp rocks, broken glass, or other objects which could cut or puncture the pipe. Where such conditions exist, suitable bedding (sand) and backfill must be provided.
- Rule 14: Take special care to prevent coal tar type coatings or petroleum base tape from contacting the plastic pipe; it can cause plastic pipe to deteriorate.
- Rule 15: Static electricity can ignite a flammable gas-air atmosphere. When working with plastic pipe of any kind where there is (or there may be) the possibility of a flammable gas-air atmosphere, take the following precautions:
 - Use a grounded wet tape conductor wound around, or laid in contact with, the entire section of the exposed piping.
 - If gas is already present, wet the pipe starting from the ground end with a very dilute water and detergent solution. Apply tape immediately and leave it in place.
 - Wet the tape occasionally with water. Where temperatures are below freezing (0°C/32°F), add glycol to the water to maintain tape flexibility. Ground the tape with a metal pipe driven into the ground.
 - <u>Do not vent gas using an ungrounded plastic pipe or tubing</u>. Even with grounded metal piping, venting gas with high scale or dust content could generate an electric charge in the gas itself and an arc could result from the dusty gas cloud back to the pipe and ignite the gas. Vent gas only at a downwind location remote from people or flammable material.
 - Note: Dissipating the static charge buildup with wet rags, a bare copper wire, or other similar techniques may not be as effective as the above procedure. In all cases, use appropriate safety equipment such as flame resistant and static free clothing, breathing apparatus, etc.

REPAIR METHODS - PLASTIC AND METAL

Replacement of gas lines and repair of leaks are highly specialized and potentially hazardous operations, persons with adequate training and certification only should attempt them. Only maintenance personnel with such training, experience, and certification should attempt repair of gas leaks or replacements of gas lines.

Leaks in service lines or mains may be repaired by cutting out a short length of pipe containing the leak and replacing it with a new segment of pipe. The pipe segment is attached to the existing line with couplings at each end. Remember that written procedures are required to be followed for each joint made. The proper procedures can be obtained from the manufacturer of the coupling.

Small leaks in steel service lines or mains, such as those resulting from corrosion pitting, are to be repaired with a steel band clamp applied directly over the leak. All bare metal pipes and fittings that are installed below ground must be properly coated and cathodically protected before backfilling. If several leaks are found and extensive corrosion has taken place, the most effective solution may be to replace the entire length of pipe that has deteriorated. The normal installation practices must be followed when performing more extensive repairs. They include priming and wrapping of all bare metallic piping and fittings, proper grading of lines to the main, cathodic protection, etc.

Leaking metal pipe can often be replaced by inserting PE pipe manufactured according to ASTM D2513 in the old line and making the appropriate connections at both ends. Again, operators are cautioned that allowance for thermal expansion and contraction must be made at lateral and end connections. Some of the PE pipe manufacturer's manuals include details for the proper techniques to install their products by insertion.

The most prevalent cause of breaks or leaks in plastic pipes are third-party damage. This is usually caused by an excavator breaking or cutting the pipe while digging. Plastic pipes are more vulnerable to such breaks than steel pipe. The lower strength of plastic pipe, however, is not necessarily a disadvantage. For example, if digging equipment hooks and pulls a steel pipe it may not break; however, the steel pipe may be pulled loose from a connection at some distance from the digging. The resulting leaks could go undetected for a period of time and may result in a serious incident. Although there is no assurance that the plastic pipe will not pull out, it is more likely to break at the point of digging. Then the break can be easily detected and repaired.

After a leak has been repaired, a soap-bubble test must be conducted. Replaced main and services must be pressure tested for leaks.

Again, it should be emphasized that all sources of ignition should be kept away from the leak repair area. MATCHES SHOULD NEVER BE USED TO DETECT A GAS LEAK or to test the adequacy of a repair job.

PROPER LOCATION AND DESIGN OF CUSTOMER METER AND REGULATOR SETS

Before locating customer meters and regulators, these points must be considered:

- 1. accessibility,
- 2. protection of meter sets from damage, and
- 3. protection of people from release of gas at the meter set.

The next section gives the regulations covering location of meters and regulators. Guidelines are given for compliance with 49 CFR Part 192.

CUSTOMER METERS AND REGULATORS: LOCATION (49 CFR 192.353)

Install meters and service regulators in a readily accessible location. Protect the meters and regulators from corrosion and other damage. Install meters outside wherever possible.

If personnel install a service regulator in a building, put it as close as practical to the point of service entering the building. The regulator must be vented to the outside.

If a meter is installed in a building, it must be located in a ventilated place. It must be more than 3' from any source of ignition or any source of heat which might damage the meter.

It is best to locate the upstream regulator (in a series) outside the building. However, regulators may be located in a separate metering or regulating building.

CUSTOMER METERS AND REGULATORS: PROTECTION FROM DAMAGE (49 CFR 192.355)

<u>Protection from vacuum or backpressure</u>. If any customer's equipment might create either a vacuum or a backpressure, then a device must be installed to protect the gas system.

Service regulator vents & relief vents. The outside terminal of each service regulator vent & relief vent must be:

- rain and insect resistant
- located where gas from the vent can escape freely into the atmosphere. Vent it 3 feet or more away from any opening into the building; and
- protected from water damage in areas where flooding may occur. (Put it where it will not be under water in a flood.)

The meters and regulators must be installed in order to minimize stress upon connecting piping. Each regulator that is designed to release gas in its operation must be vented to the outside atmosphere at least 3' from an opening into a building. Each pit or vault in a road, driveway, or parking area that houses a customer's meter, or regulator must be able to support the vehicle traffic that could use that road, driveway, or parking area.

CUSTOMER METER INSTALLATIONS: OPERATING PRESSURE (49 CFR 192.359)

A meter may not be used at a pressure that is more than 67% of the manufacturer's shell test pressure (0.67 x shell test pressure).

Each newly installed meter manufactured after November 12, 1970, must have been tested to a minimum of 10 psig.

SERVICE LINES: LOCATION OF VALVES (49 CFR 192.365)

- <u>Relation to regulator or meter</u>. Each service-line valve must be installed upstream of the regulator. If there is no regulator, install the valve upstream of the meter.
- <u>Outside valves</u>. Each service line must have a shut-off valve in a readily accessible location that, if feasible, is outside of the building.
- <u>Underground valves</u>. Each underground service line valve must be located in a covered durable curb box or standpipe that allows ready operation of the valve. <u>The box or standpipe must not put stress on the</u> <u>service line</u>.

Services should not be installed under buildings or mobile homes. If a service is installed under a building, it <u>must</u> be encased in a gas-tight conduit. This conduit must vent to the outside to a point where gas would not be a hazard and extend above ground, terminating in a rain and insect resistant fitting.

COMMON PROBLEMS TO WATCH FOR AT SERVICE RISER AND HOUSE REGULATORS

- <u>Regulator vandalism or damage</u>. This can be very hazardous. If the regulator fails to function for any reason, high-pressure gas may enter appliances. Tall flames at the burner or escape of gas could cause a fire or explosion.
- <u>Obstructed vents</u>. The vent on the regulator should be free of any obstructions. A wire screen installed at
 the vent should prevent the accumulation of dirt, the intentional insertion of foreign objects by children, or
 the build-up of insect nests (e.g., wasp nests). If the screen is removed, a new one must be inserted in its
 place. A non-functioning vent could cause regulator failure and thus present a serious fire hazard within
 the residential unit. The vent should be pointed down and away from windows and air intake.
- <u>Tenant move out</u>. The valve on the meter riser should be equipped with a locking device to be controlled by authorized personnel only. When tenants move out, the gas is shut off and locked until new tenants move in. The locking device on the shutoff valve also allows the repair of appliances without fear of the gas being accidentally turned on.

- <u>Riser misuse</u>. The tenants or customers should not be allowed to use the riser and its components for other purposes. Never use as an anchor for laundry lines, plant supports, or bicycle racks.
- <u>Corrosion</u>. Check for corrosion on the service riser at ground level.

CHAPTER 14 – Maximum Allowable Operating Pressure (MAOP)

The following items from ONG serve to document the Maximum Allowable Operating Pressures (MAOPs) of the OSU system.

OKLAHOMA NATURAL GAS

May 23, 1996



RECEIVED OKLA.CORP.COMM.

MAY 28 1996

PIPELINE SAFETY DEPT.

Ms. Tracy Rowlett Oklahoma Corporation Commission Pipeline Safety Department, Room 681 Jim Thorpe Building 2101 North Lincoln Boulevard Oklahoma City, OK 73105

Dear Ms. Rowlett:

OSU MAOP CONFIRMATION-SMALL GRAINS COMPLEX

I have provided you with the following:

• A copy of the Regulator and Relief Valve Selection (Form 761) for the measurement station at the OSU Small Grains Complex.

• A copy of the Regulator Installation or Removal (Form 502) for the installation of the Sprague CL-34 regulator. This document confirms the date of installation of the regulator.

As can be seen on the Form 761 the outlet set pressure of the Sprague CL-34 regulator is 10. 3 psig.

If you have questions regarding this matter, telephone me at (918) 588-7412.

Sincerely, J. T. Woffdra

Staff Engineer - Regulatory Compliance

Enclosures c: R. L. Clymer w/o enclosures R. L. Gambrell w/o enclosures

Appendix I-2

OKLAHOMA NATURAL GAS COMPANY A DIVISION OF ONEOK Inc. 100 WEST FIFTH STREET, TULSA, OK 74103-4298 P.O. BOX 871, TULSA, OK 74102-0871 (918) 588-7000 • FAX (918) 588-7273

THIS FORM TO BE ATTACHED TO EACH FORM 432 AND/OR JOE			TION	
REGULATOR AND RELIEF VALVE SELECTION			ORDER NUMB	ER
ATION DESCRIPTION	TOWN	ztev	EXISTING REG.	;
O.S.IL. Small Grains	ATLAS PAGE		PROPOSE	
West 6th, Near Devon Rd.	SEC T	R	REG.	
REGULATOR INFO	RMATION			
THIS SETTING IS:	SERVICE LINE		Two Stage First	ZND 2ND
LOAD DESCRIPTION			Cut Monitor Se	etting
(emmercial.			Monitor Reg.	Control Reg.
REGULATION IS UPSTREAM DOWNSTREAM	M OF METER(S)		Parallel F Primary	Runs
NORMAL OPERATING RANGE DATA	W OF METER(S)		Reg.	Stand-by Reg.
Maximum	Minimum	Re Isc	gulator Supplie blated System	** 🛛
Hourly Load Mcfh	<u> </u>	Pre	essure of conne	-
Inlet Pressure psig	<u> </u>	Inla	Design (2) t <u>60</u> psig	
Outlet Pressure (1) 0.3 oz psig	<u>10.3</u> . psig	Out	let <u>10.4</u> psig	<u>60 psig</u> 10.4 ₀₂
Porulating Capacity Meth	<u>/5.4</u> Mcfh		psig	psig
and Model No. Some Clarka Bo		l		
and Model No. Spraque C.134-2 Bo	dy Size 2"	I S	TANDARD DA	ATA
Opraque (1)4-2 bo		(1) Set	TANDARD De pressure to be :	5.333 oz.
Ice Size 56" Spring Size Man Prior RELIEF VALVE INFORMATION	dy Size 2" K Factor 700) (1). Set (9.2	pressure to be : 36"wc) for all	5.333 oz.
Relieves above regulator only		(1), Set (9.2 Reg (2) Desi	pressure to be : 36"wc) for all ulators. ign pressure to	5.333 oz. LP Service
Relieves above regulator only Relieves regulators in this setting		(1), Set (9.2 Reg (2) Desi of a	pressure to be : 36"wc) for all ulators. ign pressure to range below.	5.333 oz. LP Service
Ice Size Spring Size Marage Relieves above regulator only Relieves Relieves to regulators in this setting	K Factor 700	(1), Set (9.2 Reg (2) Desi of a LP	pressure to be : 36"wc) for all ulators. ign pressure to range below. 2 to 8 oz.	5.333 oz. LP Service be maximun
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$		(1), Set (9.2 (2) Desi of a LP MJ	pressure to be : 36"wc) for all ulators. ign pressure to range below. 2 to 8 oz. P. (A)-Less thar (B)-12 to 60	5.333 oz. LP Service be maximun n 12 psig psig
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\frac{1}{(8) = Qf} cfh$	(1), Set (9.2 (2) Desi of a LP MJ	pressure to be : 36"wc) for all ulators. ign pressure to range below. 2 to 8 oz. P. (A)-Less thar (B)-12 to 60 60 to 125 psig	5.333 oz. LP Service be maximun n 12 psig psig
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	K Factor 700	(1), Set (9.2 (2) Desi of a LP MJ	pressure to be : 36"wc) for all ulators. ign pressure to range below. 2 to 8 oz. P. (A)-Less thar (B)-12 to 60 60 to 125 psig . (A)-125 to 50 (B)-500 to 800	5.333 oz. LP Service be maximun n 12 psig psig g 0 psig 0 psig 0 psig
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\frac{1}{(8) = Qf} cfh$	(1), Set (9.2 (2) Desi of a LP MJ	pressure to be : 36"wc) for all ulators. ign pressure to range below. 2 to 8 oz. P. (A)-Less thar (B)-12 to 60 60 to 125 psig . (A)-125 to 50	5.333 oz. LP Service be maximun n 12 psig psig g 0 psig 0 psig 0 psig
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\frac{26,040}{(8) = Qt}$ cfh	(1), Set (9.2 Reg (2) Desi of a LP MJ I.P. HP	pressure to be : 36"wc) for all ulators. ign pressure to range below. -2 to 8 oz. P. (A)-Less thar (B)-12 to 60 60 to 125 psig. .(A)-125 to 50 (B)-500 to 80 (C)-Over 800 imum build-up	5.333 oz. LP Service be maximun n 12 psig psig 0 psig 0 psig psig on outlet
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\frac{\mathbf{E} \mathbf{K} \operatorname{Factor}}{(8) = Qt} \frac{700}{\text{cfh}}$ $\frac{26_{10}40}{(8) = Qt} \text{cfh}$ $\frac{26_{10}40}{\text{cfh}} \text{cfh}$	(1), Set (9.2 Reg (2) Desi of a LP MJ I.P. HP (3) Max. syste	pressure to be : 36"wc) for all ulators. ign pressure to range below. 2 to 8 oz. P. (A)-Less thar (B)-12 to 60 60 to 125 psig .(A)-125 to 50 (B)-500 to 800 (C)-Over 800	5.333 oz. LP Service be maximun n 12 psig psig 0 psig 0 psig psig on outlet
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\frac{1}{(8) = Qt} \frac{700}{cth}$ $\frac{26_{10}40}{cth} cth$ $\frac{15}{26} qt$ $\frac{1}{26} pt$	(1), Set (9.2 Reg (2) Desi of a LP MJ I.P. HP (3) Max: syste for: LP.	pressure to be : 36"wc) for all ulators. ign pressure to range below. -2 to 8 oz. P. (A)-Less thar (B)-12 to 60 -60 to 125 psig (A)-125 to 50 (B)-500 to 800 (C)-Over 800 imum build-up m must NOT E -14 oz. (24.20"	5.333 oz. LP Service be maximun n 12 psig psig 0 psig 0 psig 0 psig psig on outlet EXCEED, 'wc)
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\frac{\mathbf{E} \mathbf{K} \operatorname{Factor}}{(8) = Qt} \frac{700}{\text{cfh}}$ $\frac{26_{10}40}{(8) = Qt} \text{cfh}$ $\frac{26_{10}40}{\text{cfh}} \text{cfh}$	(1), Set (9.2 Reg (2) Desi of a LP MJ I.P. HP (3) Max: syste for: LP.	pressure to be : 36"wc) for all ulators. ign pressure to range below. 2 to 8 oz. P. (A)-Less thar (B)-12 to 60 60 to 125 psig . (A)-125 to 50 (B)-500 to 800 (C)-Over 800 imum build-up m must NOT E -14 oz. (24.20" P. (A)-MAOP +	5.333 oz. LP Service be maximun n 12 psig psig 0 psig 0 psig on outlet EXCEED, 'wc) 50%
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\frac{1}{(8) = Qt} \frac{700}{cth}$ $\frac{26_{10}40}{cth} cth$ $\frac{15}{26} qt$ $\frac{1}{26} pt$	(1), Set (9.2 Reg (2) Desi of a LP MJ LP. HP (3) Max: syste for: LP. M.P LP.	pressure to be : 36"wc) for all ulators. ign pressure to range below. -2 to 8 oz. P. (A)-Less thar (B)-12 to 60 -60 to 125 psig. (A)-125 to 500 (B)-500 to 800 (C)-Over 800 imum build-up imum build-up imum build-up -14 oz. (24.20" -(A)-MAOP + (B)-MAOP + 10%	5.333 oz. LP Service be maximun a 12 psig psig 0 psig 0 psig psig on outlet EXCEED, 'wc) 50% 6.0 psig
$\frac{1 \text{ Ce Size} \qquad 9 \text{ Spring Size} \qquad \text{Marke } - \qquad \text{Hist} \text{ explosive}}{\text{ReLIEF VALVE INFORMATION}}$ $\frac{\text{Relieves above regulator only}}{\text{Relieves } - \qquad \text{regulators in this setting}}$ $\frac{\text{Regulator}}{\text{Failure}} \qquad (14.4 + \frac{(5)}{(5)}) (\frac{-700}{(6) = Cq}) (1.29) = \\ (14.4 + \frac{(5)}{(5)}) (\frac{-700}{(6) = K}) (\frac{-700}{(7)}) \\ (6) = K = \\ - \\ - \\ - \\ - \\ - \\ - \\ - \\ - \\ - \\$	$\frac{\mathbf{z} \cdot \mathbf{K} \cdot \mathbf{Factor}}{(8) = \mathbf{Q}t} \frac{\mathbf{f} \cdot \mathbf{C}}{\mathbf{C}th}$ $\frac{\mathbf{z} \cdot \mathbf{G}}{(8) = \mathbf{Q}t} - \mathbf{C}th$ $\frac{\mathbf{z} \cdot \mathbf{G}}{(8) = \mathbf{Q}t} - \mathbf{C}th$ $\frac{\mathbf{C}th}{(8) = \mathbf{Q}t} - \mathbf{C}th$ $\frac{\mathbf{f} \cdot \mathbf{G}}{(8) = \mathbf{Q}t} - \mathbf{C}th$	(1), Set (9.2 Reg (2) Desi of a LP MJ LP. HP (3) Max: syste for: LP. M.P LP.	pressure to be : 36"wc) for all ulators. ign pressure to range below. -2 to 8 oz. P. (A)-Less thar (B)-12 to 60 60 to 125 psig. .(A)-125 to 50 (B)-500 to 80 (C)-Over 800 : imum build-up imum build-up imum build-up -14 oz. (24.20" P. (A)-MAOP + (B)-MAOP + 10% -MAOP + 10%	5.333 oz. LP Service be maximun a 12 psig psig 0 psig 0 psig psig on outlet EXCEED, 'wc) 50% 6.0 psig
$\frac{1 \text{ ce Size} \qquad 9 \text{ g} \qquad \text{Spring Size } \underset{\text{marge}}{\text{marge}} = \qquad \begin{array}{c} \text{Hist} \underset{\text{cess}}{\text{marge}} = \\ \hline \\ \text{Relieves above regulator only} \\ \hline \\ \text{Relieves } \qquad \text{regulators in this setting} \\ \hline \\ \text{Regulator} \qquad (14.4 + \underbrace{60}_{(5)}) (\underbrace{-700}_{(6) = C9}) (1.29) = \\ \hline \\ \text{Failure} \qquad (14.4 + \underbrace{60}_{(5)}) (\underbrace{-700}_{(6) = K}) \\ \hline \\ \text{capacity} \qquad (14.4 + \underbrace{60}_{(5)}) (\underbrace{-700}_{(6) = K}) \\ \hline \\ \text{Less: Capacity of Internal} \\ \hline \\ \text{Relief Valve, If any} \\ \hline \\ \\ \text{Required Relief Valve Capacity} \\ \hline \\ \\ \text{Maximum Relief Valve Inlet Pressure} \\ \hline \\ \hline \\ \text{Make and Model} \\ \hline \\ \hline \\ \hline \\ \hline \\ \hline \\ \hline \\ \text{Capacity} \\ \hline \\ \hline \\ \hline \\ \text{Z7, } \\ \hline \\ \end{array} \\ \hline \\ \hline \\ \end{array} $	$\frac{\mathbf{K} \operatorname{Factor}}{(8) = \operatorname{Qf}} \xrightarrow{f} cfh$ $\frac{26_{,0}40}{cfh} cfh$ $\frac{15}{2} \operatorname{Qf} cfh$	(1), Set (9.2 Reg (2) Desis of a LP MJ LP HP (3) Max: syste for: LP. M.P LP. HP. (4) LP. F	pressure to be : 36"wc) for all ulators. ign pressure to range below. -2 to 8 oz. P. (A)-Less thar (B)-12 to 60 -60 to 125 psig. (A)-125 to 500 (B)-500 to 800 (C)-Over 800 imum build-up imum build-up imum build-up -14 oz. (24.20" -(A)-MAOP + (B)-MAOP + 10%	5.333 oz. LP Service be maximun a 12 psig psig 0 psig 0 psig 0 on outlet EXCEED, 'wc) 50% 6.0 psig up to 75%
Ice Size Spring Size Marker Filer Relieves Relieves above regulator only Relieves regulator only regulators in this setting Required $(14.4 + (5)) (-(6) = Cq) (1.29) =$ Failure $(14.4 + (5)) (-(6) = Cq) (7) =$ (7) (7) = Capacity $(14.4 + (60)) (-700) (-(700) (7) =(6) = K =$ $(14.4 + (60)) (-(700) (7) =(6) = K =$ Capacity $(14.4 + (60)) (-(700) (-(700)) (-(700) (7) =(14.4 + (60)) (-(700) (-(700)) (-(700) (7) =(14.4 + (60)) (-(700) (-(700)) (-(700) (-(700)) (-(700)) (-(700) (-(700)) (-(700)) (-(700) (-(700)) (-(700) (-(700)) (-(700) (-(700)) (-(700)) (-(700) (-(700)) (-(700) (-(700)) (-(700) (-(700)) (-(700) (-(700)) (-(700) (-$	$\frac{\mathbf{z} \mathbf{k} \operatorname{Factor}}{(8) = Qt} \frac{700}{\text{cth}}$ $\frac{2600}{(8) = Qt} \text{cth}$ $\frac{2600}{(8) = Qt} \text{cth}$ $\frac{15}{200} \text{cth}$ $\frac{15}{200} \text{cth}$ $\frac{12}{200} \text{cth}$ $\frac{12}{200} \text{cth}$	(1), Set (9.2 Reg (2) Desi of a LP MJ LP. HP (3) Max: syste for: LP. M.F LP. HP. (4) LP. F (20.7	pressure to be : 36"wc) for all ulators. ign pressure to range below. -2 to 8 oz. (A)-Less thar (B)-12 to 60 60 to 125 psig. (A)-125 to 50 (B)-500 to 80 (C)-Over 800 imum build-up imum build-up imum build-up imum build-up (A)-MAOP + (B)-MAOP + (B)-MAOP + 10% of SMYS Relief must begi 6" wc)	5.333 oz. LP Service be maximun n 12 psig psig 0 psig 0 psig 0 on outlet EXCEED, 'wc) 50% 6.0 psig up to 75% in at 12 oz.
Ice Size Spring Size Orange Filer RIG: χ Relieves	$\frac{\mathbf{z} \mathbf{k} \operatorname{Factor}}{(8) = Qt} \frac{700}{\text{cth}}$ $\frac{2600}{(8) = Qt} \text{cth}$ $\frac{2600}{(8) = Qt} \text{cth}$ $\frac{15}{200} \text{cth}$ $\frac{15}{200} \text{cth}$ $\frac{12}{200} \text{cth}$ $\frac{12}{200} \text{cth}$	(1), Set (9.2 Reg (2) Desi of a LP MJ LP. HP (3) Max: syste for: LP. M.F LP. HP. (4) LP. F (20.7	pressure to be : 36"wc) for all ulators. ign pressure to range below. -2 to 8 oz. (A)-Less thar (B)-12 to 60 -60 to 125 psig. (A)-125 to 50 (B)-500 to 800 (C)-Over 800 imum build-up imum build-up imum build-up imum build-up (A)-MAOP + (B)-MAOP + (B)-MAOP + 10% -MAOP + 10% of SMYS Relief must begi 6" wc) eral Office App	5.333 oz. LP Service be maximun a 12 psig psig 0 psig 0 psig 0 on outlet EXCEED, 'wc) 50% 6.0 psig up to 75% in at 12 oz. rovals
Ice Size Spring Size Marker Filer Relives Relives above regulator only Relieves Relives in this setting Regulator $(14.4 + (5)) (-(6) = Cq) (1.29) =$ Failure $(14.4 + (5)) (-(6) = Cq) (7) =$ Failure Capacity $(14.4 + (60)) (-(700)) $	$\frac{\mathbf{z} \mathbf{k} \operatorname{Factor}}{(8) = Qt} \frac{700}{\text{cth}}$ $\frac{2600}{(8) = Qt} \text{cth}$ $\frac{2600}{(8) = Qt} \text{cth}$ $\frac{15}{200} \text{cth}$ $\frac{15}{200} \text{cth}$ $\frac{12}{200} \text{cth}$ $\frac{12}{200} \text{cth}$	(1), Set (9.2 Reg (2) Desi of a LP MJ LP. HP (3) Max: syste for: LP. M.P LP. HP. (4) LP.F (20.7 Gene	pressure to be : 36"wc) for all ulators. ign pressure to range below. -2 to 8 oz. P. (A)-Less thar (B)-12 to 60 -60 to 125 psig. (A)-125 to 50 (B)-500 to 800 (C)-Over 800 imum build-up imum build-up imum build-up imum build-up m must NOT E -14 oz. (24.20" -14	5.333 oz. LP Service be maximun n 12 psig psig 0 psig 0 psig 0 on outlet EXCEED, 'wc) 50% 6.0 psig up to 75% in at 12 oz.
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	GOFI
Form 502 Rev. 3-63 REGULATOR IN	STALLATION OR REMOVAL
	Date of { Installation Removal }
LocationW. Hwy 51 - Small Grains C	
Controls From C.P.M.P.	Controls ToSmall Grains Complex
Inlet Pressure 30-45#	Outlet Pressure 10# Site Size
Housing-Kind & Size OPEN - ON	
Inlet Gauge Make	Ind Rec Range
Outlet Gauge Make	Ind Rec Range
By Pass Size Type of	of CutoffStops
Safety Valve Make Fisher 289-	
Set to Pop at Leaks At	12# Pops At 15# Reseats At 12#
Location of Safety Value ON iNlet be-	tween regulator & Meter
Other Attachments, Describe	
/	Pass Stops Not Connected
2" Balon VAlue IL	nder RIV (Cocked)
From Stock At	Placed in Stock At
Complete Make Sprague C	OR { JOB WORK } ORDER No Description of Regulator 24.34-2Type of LoadingC.L.Pr
Complete Make Sprague C Mfg Serial No None	2.34-2Type of LoadingC.L.P.
Complete Make	Description of Regulator 24.34-2 Type of LoadingC.L.A. Co. NoCo. No Type ConScFlange Rating
Complete Make	Description of Regulator 24.34-2Type of Loading
Complete Make	Description of Regulator 24.34-2Type of Loading Co. No Co. No Type Con Sc. Flange Rating No. Bolts Size No. Bolts Size
Complete Make	Description of Regulator 24.34-2Type of Loading
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Complete Make	Description of Regulator 24.34-2Type of Loading Co. No
Complete Make	Description of Regulator 24.34-2Type of Loading Co. No
Complete Make	Description of Regulator 24.34-2Type of Loading Co. No Type Con Sc. Flange Rating No. Bolts Size No. Bolts Size No. Bolts Single X Type Seat Soft 289-H (5-14# sprix I'' Type & Size Dehydrator Pot
Complete Make	Description of Regulator 24.34-2Type of Loading Co. No Type ConSc Flange Rating No. Bolts No. Bolts Lever Length Single 2# Inlet To # Inlet To 289-H CoRAuge_ Main Spring
Complete Make	Description of Regulator 24.34-2Type of Loading Co. No Type ConSc Flange Rating No. BoltsSize No. BoltsSize Lever Length Single X Type Seat Soft 2# Inlet To 30-45# Outlet 10.4# 289-H (5-14# Spring 289-H (5-14# Spring) ORAuge Main Spring Black Pilot Spring 3-30
Complete Make	Description of Regulator 24.34-2Type of Loading Co. No Type ConSc Flange Rating No. Bolts No. Bolts Lever Length Single 2# Inlet To # Inlet To 289-H CoRAuge_ Main Spring
Complete Make	Description of Regulator 24.34-2Type of Loading Co. No Type ConSc Flange Rating No. BoltsSize No. BoltsSize Lever Length Single X Type Seat Soft 2# Inlet To 30-45# Outlet 10.4# 289-H (5-14# Spring 289-H (5-14# Spring) ORAuge Main Spring Black Pilot Spring 3-30
Complete Make	Description of Regulator 24.34-2Type of Loading Co. No Type ConSc Flange Rating No. BoltsSize No. BoltsSize Lever Length Single X Type Seat Soft 2# Inlet To 30-45# Outlet 10.4# 289-H (5-14# Spring 289-H (5-14# Spring) ORAuge Main Spring Black Pilot Spring 3-30
Complete Make	Description of Regulator 24.34-2Type of Loading Co. No Type ConSc Flange Rating No. BoltsSize No. BoltsSize Lever Length Single X Type Seat Soft 2# Inlet To 30-45# Outlet 10.4# 289-H (5-14# Spring 289-H (5-14# Spring) ORAuge Main Spring Black Pilot Spring 3-30
Complete Make	Description of Regulator 24.34-2Type of Loading Co. No Type ConSc Flange Rating No. BoltsSize No. BoltsSize Lever Length Single X Type Seat Soft 2# Inlet To 30-45# Outlet 10.4# 289-H (5-14# Spring 289-H (5-14# Spring) ORAuge Main Spring Black Pilot Spring 3-30
Complete Make <u>Sprigue C</u> Mfg Serial No. <u>None</u> Size Inlet <u>2"</u> Size Outlet <u>2"</u> Diameter Bolt Circle Inlet Diameter Bolt Circle Outlet Size Diaphra <u>Size</u> <u>Std</u> Size Valves <u>Std</u> Size Valves <u>Std</u> Size Valves <u>Std</u> Safety Valve Make <u>Fisher</u> Type of Safety Valve <u>Spriwa</u> Size Other Descriptive Information <u>9-1-76</u> <u>Nomewood Fisher</u> <u>99</u> <u>12.St alled Sprigue C.L.</u> <u>34-2</u>	Description of Regulator 24.34-2Type of LoadingC.L.P. Co. No Type ConScFlange Rating No. BoltsSize No. BoltsSize Lever Length Lever LengthType Seat Soft Iot 2# Inlet To 30-45#OutlerO.4# 289-HJO.4# 289-HSpring ORA uge Main Spring Size Dehydrator Pot ORA uge Main Spring
Complete Make <u>Springue C</u> Mfg Serial No. <u>None</u> Size Inlet <u>2"</u> Size Outlet <u>2"</u> Diameter Bolt Circle Inlet Diameter Bolt Circle Outlet Size Diaphra <u>Size</u> Std Size Valves <u>Std</u> Size Valves <u>Std</u> Size Valves <u>Std</u> Safety Valve Make <u>Fisher</u> Type of Safety Valve <u>Spring</u> Size Other Descriptive Information <u>9-1-70</u> Nomerod Fisher <u>99</u> <u>12:St alled Springene C.L. 34-2</u>	Description of Regulator 24.34-2Type of Loading Co. No Type ConScFlange Rating No. BoltsSize No. BoltsSize Lever Length Single X Type Seat Soft 2# Inlet To 30-45# Outlet 10.4# 289-H (5-14# Spring 289-H (5-14# Spring) ORAuge Main Spring Black Pilot Spring 3-30
Complete Make <u>Springue C</u> Mfg Serial No. <u>None</u> Size Inlet <u>2"</u> Size Outlet <u>2"</u> Diameter Bolt Circle Inlet Diameter Bolt Circle Outlet Size Diaphra <u>Size</u> Std Size Valves <u>Std</u> Size Valves <u>Std</u> Size Valves <u>Std</u> Safety Valve Make <u>Fisher</u> Type of Safety Valve <u>Spring</u> Size Other Descriptive Information <u>9-1-70</u> Nomerod Fisher <u>99</u> <u>12:St alled Springene C.L. 34-2</u>	Description of Regulator 24.34-2Type of LoadingC.L.P. Co. No Type ConScFlange Rating No. BoltsSize No. BoltsSize Lever Length Lever LengthType Seat Soft Iot 2# Inlet To 30-45#OutlerO.4# 289-HJO.4# 289-HSpring ORA uge Main Spring Size Dehydrator Pot ORA uge Main Spring



May 8, 1996



RECEIVED OKLA. CORP. COMM.

MAY 1 3 1996

PIPELINE SAFETY DEPT.

Ms. Tracy Rowlett Oklahoma Corporation Commission Pipeline Safety Department, Room 681 Jim Thorpe Building 2101 North Lincoln Boulevard Oklahoma City, OK 73105

Dear Ms. Rowlett:

OSU MAOP CONFIRMATION

I have provided you with the following:

- A copy of the Regulator and Relief Valve Selection (Form 761) for the Measurement Station 65-708.
- A copy of the Completion Report (Form 702) for construction on the rebuild of Measurement Station 65-708. This document confirms date of installation on the existing Rockwell regulator.
- A copy of the Regulator and Relief Valve Selection (Form 761) for the Measurement Station 91-631.

The Form 761 is the Oklahoma Natural Gas Company document of record regarding regulators and relief valves at commercial and industrial meter settings and at district regulator settings. As can be seen on the attached documents, the Form 761 lists the regulator and relief valve specifications such as size, inlet pressure, capacity, and outlet set points. By Oklahoma Natural procedures, if any component at a meter and regulator station is altered, or if there is an increase of the regulator inlet or outlet pressure, then a new Form 761 must be completed to reflect the changes. After researching our files, we are confident that the attached Form 761s are the most recent and no significant revisions have since been made to the regulators and relief valves.

Appendix I-5

OKLAHOMA NATURAL GAS COMPANY A DIVISION OF ONEOK Inc. 100 WEST FIFTH STREET, TULSA, OK 74103-4298 P.O. BOX 871, TULSA, OK 74102-0871 (918) 588-7000 • FAX (918) 588-7273

Ms. Tracy Rowlett Page 2 May 8, 1996



The attached Form 761 for Station 91-631 accurately reflects the current delivery pressure of 35 psig. However, the Form 761 for Station 65-708, listing the regulator outlet pressure as 35 psig, is no longer correct. Approximately, ten years ago the delivery pressure through this meter setting was reduced to its current level of 32 psig.

Prior to serving customers with elevated pressure, Oklahoma Natural personnel review the customer's piping system to ensure that materials and construction methods meet the appropriate standards. These safety inspections, in addition to the inspections performed by local building inspectors, were performed on the OSU piping systems prior to the initiation of service. The systems met Oklahoma Natural standards for customer piping and were approved to receive 35 psig. A survey of records and Stillwater area personnel indicates no subsequent safety problems on the OSU system. For these reasons, we recommend that the current pressures on the two systems be considered as the MAOP.

If you have questions regarding this matter, telephone me at (918) 588-7412.

Sincerely, Wofford т.

Staff Engineer - Regulatory Compliance

Enclosures c: R. L. Clymer w/o enclosures R. L. Gambrell w/o enclosures

Appendix I-6

THIS FORM TO BEAL AGHED TO EACH FORM 432 AND/OR JOB ORDER FOR REGULATOR	
REGULATOR AND RELIEF VALVE SELECTION	JOB ORDER NUMBER
ATION DESCRIPTION TOWN Stillwa	existing REG.
MEGeorge West of Monroe ATLASPAGE	PROPOSED
O.S.U. C. Ampus (Vet Village) SECT_	R
REGULATOR INFORMATION	
THIS SETTING IS:	Two Stage Setting First 2ND
LOAD DESCRIPTION (South Regulator)	Cut Cut Cut Monitor Setting
Residential & Commercial 47.1 MCFH	Monitor Control Reg. Reg.
REGULATION IS UPSTREAM MOF METER(S)	Parallel Runs Primary Reg. Stand-by Reg.
NORMAL OPERATING RANGE DATA <u>Maximum</u> Minimum	Regulator Supplies Isolated System
Hourly Load 47.1 Mcfh 20 Mcfh	Pressure of connecting lines
Inlet Pressure psig 50 psig	Inlet <u>Design (2)</u> <u>MAO</u> <u>Inlet</u> <u>60</u> psig <u>60</u> psig
Outlet Pressure (1)35-oz psig35-oz psigRegulating Capacity148Mcfh113Mcfh113Mcfh	Outlet 60 02. 60 02.
	psig psig
and Model No. Rockwell 441-575 Body Size 2"	STANDARD DATA
دو Size <u>الجامعة</u> (Brown) CFor K Factor 4270 RELIEF VALVE INFORMATION	= (1), Set pressure to be 5.333 oz. (9.236"wc) for all LP Service
Relieves above regulator only	(2) Design pressure to be maximum
Relieves regulators in this setting	of a range below. LP2 to 8 oz.
Regulator $(14.4 + (5))(-(6) = Cg)(1.29) = -(6) = Cfh$	M.P. (A)-Less than 12 psig
Fallure	(B)-12 to 60 psig I.P60 to 125 psig
Capacity $(14.4 + \frac{60}{(5)}) (\frac{4370}{(6) = \kappa})$ OR $(150, 8.44)$	HP. (A)-125 to 500 psig (B)-500 to 800 psig
Less: Capacity of Internal	(C)-Over 800 psig
Relief Valve, If any	(3) Maximum build-up on outlet
Horizon Deli GV I. L. L. D. L.	system must NOT EXCEED, for:
Palief Value Set Deserves	LP14 oz. (24.20" wc) M.P. (A)-MAOP + 50%
Make and Model (187, 345 CFH) (19, 380 CFH)	(B)-MAOP + 6.0 psig
(Imerican axial Flow + 1x1/2 Farris 1875-R	HPMAOP + 10% HPMAOP + 10% up to 75%
Capacity 206, 725 TOTACT Inlet and Outlet Size Z" X Z"	of SMYS
Type of loading Weight Lever & Weight Pilot	(4) LP. Relief must begin at 12 oz. (20.76" wc)
Regulator Failure Capacity Formula: PI x Cg x 1.29 = Qf OR $\frac{KPI}{2}$ = Qf	General Office Approvals
liator Valve Coefficient from Manufacturer's Data. Lor to correct spec. grav. of air(1.0) to 0.6 Nat. Gas (ar_, otal offh to be relieved at 100% open Reg. Failure	Initial Date
DISTRICT R H- OR	Meas.
Prepared By Approved	Tech. Serv
Appendix I-7	u .

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9			2"		ONG		pipe, structura			
63'				3.00	1		pipe, structura	(fames)	·····	
84'			1.4	1.68#	1		pipe, A-25 P.E.	(fence)		
42'			1"	1.68#	1		tubing pressure	(Lauce)		
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PREPARED BY Bill Holle Appendix I-9	

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Appendix I-11	

CHAPTER 15 - NG Maintenance Forms

Various Natural Gas Maintenance and Inspection Forms

KEY VALVE INSPECTION FORM

KEY VALVE INSPECTIONS are completed once per calendar year.

DATE	· · · · · ·	
Valve Number	Location	Smart Number
Problem Noted:		
Action Taken:		
DATE		
Valve Number	Location	Smart Number
Problem Noted:		
Action Taken:		
DATE		

Valve Number	Location	Smart Number
Problem Noted:		
Action Taken:		

Operator (Print Name)

Operator Signature

Thereby certify that I have inspected this valve and found it to be Acceptable Onacceptable	hereby certify that I have inspected this valve and found it to be Acceptable	Unacceptable
---	---	--------------

Inspection notes after correction of unacceptable findings:

Inspector (Print Name)

Inspector Signature

PIPE JOINING FORM

FUSION 1				
Type of Joint	Butt Fusion		Electrofusion	Metallic Weld
Items Joined				
Size and Material				
Start Time				
Electrofusion Info Only				
Fusion Time	C	lamp Time		Voltage
FUSION 2				
Items Joined				
Size and Material				
Start Time				
Electrofusion Info Only	1			
Fusion Time	C	lamp Time		Voltage
FUSION 3				
Items Joined				
Size and Material				
Start Time				
Electrofusion Info Only				
Fusion Time	C	lamp Time		Voltage
FUSION 4				
Items Joined				
Size and Material				
Start Time				
Electrofusion Info Only				
Fusion Time	C	lamp Time		Voltage
			0	
Operator (Print Name)			Operator Signature	
I hereby certify that I have insp	pected this joir	nt and found	l it to be Acceptable	Unacceptable
Inspector (Print Name) Inspector Signature				
If joint is unacceptable, action	taken to corre	ect:		
I hereby certify that I have insp	bected this joir	nt and found	I It to be Acceptable	Unacceptable
Inspector (Print Name)			Inspector Signature	
M:\DIST SYSTEMS\UTIL DIST		GAS∖NG MA	NUAL\FY25_NG-MAN	UAL\NG-MANUAL-

PRESSURE TEST FORM

DATE					
Test Station Location					
Test Station Length					
Pipe Material	Pipe Size				
Test Medium					
Time Started	Time Ended				
Pressure at Start	Pressure at End				
Reason for any line loss that occurred:					
Repairs made to correct leakage:					
Insert sketch of piping layout or make one on reverse side of this form.					

Operator (Print Name)

Operator Signature

SNIFF TEST FORM

SNIFF TESTS are completed quarterly.

DATE:

Sprec (0709)						
Odor Noted	YES	NO				
Action taken if no odor was detected.						
Plant Pathology Research Greenhouse (0689)						

Plant Pathology Research Greenhouse (0689)				
Odor Noted	YES	NO		
Action taken if no odor was det	ected.			

Greenwood School of Music (02	272)								
Greenwood School of Music (0272) Odor Noted YES NO Action taken if no odor was detected.									
Action taken if no odor was det	ected.								

Track Facility (0289)							
Odor Noted YES NO Action taken if no odor was detected. Image: Constant of the second							
Action taken if no odor was det	ected.						

SNIFF TEST FORM

SNIFF TESTS are completed quarterly.

DATE:

Alumni Center (0005)								
Alumni Center (0005) Odor Noted YES Action taken if no odor was detected.								
Action taken if no odor was dete	ected.							

Bennett Hall (0038)								
Bennett Hall (0038) Odor Noted YES NO Action taken if no odor was detected.								
Action taken if no odor was det	ected.							

Sherman Smith Training Center (0286)									
Odor Noted YES NO									
Action taken if no odor was det	ected.								

Operator (Print Name)

Operator Signature

SURVEILLANCE and PATROLLING INSPECTION FORMS

Performed twice each year for entire system. New form to be completed each day. Use the ba	ack of sheet or multiple sheets if necessary.
Date	
Vegetation and Insect Survey	
Problem area:	Action taken:
Above-Ground Corrosion Inspection	
Problem area:	Action taken:
Survey Results Notes:	

Operator (Print Name)

Operator Signature

CHAPTER 16 – PE and Metallic Pipe Joining Procedures

PLASTIC PIPE FUSION INSTRUCTIONS

METALLIC WELDING and QUALIFICATION PROCEDURES

The qualification of OSU ES welders shall be done by a recognized independent testing entity conducted in accordance with Section IX, ASME Boiler and Pressure Vessel Code. Timing for certification is as follows.

After initial qualification, a welder may not perform welding unless:

- 1. Within the preceding 15 calendar months, the welder has re-qualified, except that the welder must requalify each calendar year, or
- 2. Within the preceding 7¹/₂ calendar months, but at least twice each calendar year, the welder has had a production weld cut out, tested, and found acceptable in accordance with the qualifying test.

Welder qualification procedures from the independent testing entity shall be kept on file.

GENERAL WELDING PROCEDURES

WELDING STEEL PIPE:

All welding shall conform to ASME Section 9, with a retest every 6 months.

- 1. Welder shall use position welding with the vertical down as the direction of welding.
- 2. Each joint shall be wire brushed or use other acceptable means to remove rust, dirt, mill scale or other foreign substances before being placed in alignment for welding.
- 3. The adjoining lengths of pipe shall be accurately aligned using a suitable alignment clamp. The adjoining lengths of pipe shall be accurately spaced before welding. Under no circumstances shall metered pipe welds be allowed.
- 4. The root bead shall be applied completely around the circumference of the pipe and adequately cleaned of all scale and slag. The second bead (the hot pass) shall be applied immediately after this cleaning operation. Before the day's work is completed hot passes will be applied to all root beads. Under no circumstances will welded joints be accepted when such have been connected only by the root bead from the end of one day's work to the next. Each completed weld shall be thoroughly cleaned of slag, coating, and scale. Welded sections of pipe will not be rolled off dollies until all affected welds have cooled.
- 5. In case of cold, rainy weather, or excessive winds, the operator shall provide protection for the welders while at work and care will be taken to assure that welds are not subject to sudden changes in temperature until such welds are thoroughly cooled. Welding will not be carried on when, in the judgment of the operator, the weather is unsuitable for welding operations.
- 6. If upon inspection, a weld appears defective, the welder shall cut from the line a cylinder of pipe continuing such a weld and replace it with good pipe or shall have the weld repaired to the satisfaction of the Superintendent. The following limits apply:
 - a. Cracks, regardless of their location, will not be repaired.
 - b. Defects, except cracks, which are externally exposed in the cover pass may be repaired without prior approval from the Superintendent.
 - c. Defects beneath the cover of the surface of the cover pass specifically defined, in the opinion of the Superintendent as slag inclusions, porosity or gas pockets may be repaired in compliance with API 1104 provided:
 - i. The defect can be repaired without grinding completely through the weld.
 - ii. No single area of the defect shall exceed 25 percent of the pipe circumference length. A given single area of defect may consist of one or more defects.

- iii. Adjacent areas of defects shall be separated by sound weld metal of a length not less than 7 percent of the pipe circumference length.
- iv. Before such repairs are made, such defects shall be entirely removed to clean metal by grinding in a manner acceptable to the Superintendent. All slag and scale will be removed by wire bending.
- v. Flame cutting and air carbon arc gouging will not be used for removing defects in production of tie-in welds. Air carbon arc may be used to remove defects in fabrication welds only.
- vi. When preheating is required, an area of four inches on each side of the repair shall be preheated to a minimum of 200 degrees F. and maintained during repair welding. Temperature will be checked by using a temperature indicating crayon.
- vii. All repair cavities will not be less than 2 inches in length. All repairs will be made with a minimum of two passes. The start and stop of repair passes will not be superimposed over the start and stop of the preceding repair pass.
- viii. All repairs shall meet the Standard of Acceptable Nondestructive Testing.
- ix. No further repairs will be made in these areas.

WELDING PRECAUTIONS:

The welder will take necessary precautions to ensure that no arcing occurs between the ground lead of the welding machine and the pipe of the fittings. Striking the arc on any point other than the welding grove will not be permitted. All arc burns on the pipe will be removed by cutting a cylinder of pipe continuing the arc burn and replacing it with good pipe.

Preheating will be used when welding fitting to fitting and pipe to pipe fittings, and when the internal pipe temperature is 45° or below. Preheating will also be used when the pipe, for any reason, is wet or damp. Such preheating will be accomplished by any means acceptable to the Superintendent and shall cover an area of at least four inches on each side of the weld. A minimum of 200° F. will be maintained during the welding process and will be checked by using a temperature indicating crayon.

During shutdown, the open ends of the pipe shall be securely closed, and all pipe ends raised to prevent the entrance of small animals, water or obstructions and shall not be reopened until work recommences. A suitable cover of about the same diameter as the pipe will be placed over the open ends of the tie-in sections or both ends of a long section. Any obstructions that occur must be removed by the welder to the satisfaction of the Superintendent. The line must be delivered entirely free from water, dirt, obstructions, or other foreign material.

No pup joints will be installed in the line that is less than 20" in length.

All construction tie-ins, other than those at road or stream crossings, will be made at a point level with the top of the trench, unless otherwise specified by the Superintendent.

WELDING OF SERVICE LINES:

Steel service lines are constructed with approved black pipes. The maintenance crews are provided with tools and components to cut and thread black pipe so that welding is not required for service lines except the tapping tees. Taps are welded onto the top surface of the mains. Welders who do any welding for OSU are to be tested in this type of welding.

Welding must not begin until there is enough space to allow the welder freedom of movement. The welding must not be performed during severe weather. Any flammable materials must be kept clear.

Visual inspection of all welds is expected of both the welder and any other crew members present who are qualified to visually inspect welds. A qualified welder is also considered qualified to inspect welds. The metal of the main where a branch is to be located, must be in decent shape so that it will hold up under the increased stresses due to discontinuity in the pipe material. The area on the main close to the weld must be clean and dry. The weld, when complete, should be cleaned of weld slag so that it can be inspected for undercutting and so that rough spots or excessive reinforcement can be ground off. Runs of pipe for mains are welded. The welding procedure requirements that crew members should watch out for are outlined as follows:

- 1. The only person permitted to do the welding is the one qualified.
- 2. The welder is to be looked after during welding operations. Sometimes it is important that his instructions or requests are conducted quickly and correctly.
- 3. The other crew members are allowed to help with the set-up, cleaning, scraping, and grinding. However, anyone using power tools must wear safety glasses.
- 4. The metal in the weld must be clean and dry before any welding is done.
- 5. The alignment and pre-spacing must be maintained while the root bead are made.
- 6. The weld slag and rough spots must be chipped and cleaned before the second weld is started.
- 7. The second weld should be made shortly after the root bead is completed but not while the root bead is still hot.
- 8. The weld slag and rough spots must be chipped and ground away. If this is the final weld, a visual inspection must be made to make sure there is not any undercutting and that the proper amount of reinforcement exists. Additional welds are the same as the second weld for the purpose of these instructions.

CHAPTER 17 – Line Locator User Manual

CHAPTER 18 – NG System Earthquake Plan

Oklahoma State University

Stillwater, Oklahoma



Facilities Management - Energy Services Central Plant, Bldg #0282 - 510 North Washington, Stillwater OK 74078

Distribution Systems Utilities Distribution Natural Gas System

Earthquake Plan

Revised Spring 2022

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1 – EARTHQUAKE PREPAREDNESS

DEFINITIONS

EARTHQUAKE

Earthquake is a term used to describe both sudden slip on a fault and the resulting ground shaking and radiated seismic energy caused by the slip, or by volcanic or magmatic activity, or other sudden stress changes in the earth.

FAULT

A fault is a fracture along which the blocks of crust on either side have moved relative to one another parallel to the fracture.

LIQUEFACTION

A process by which water-saturated sediment temporarily loses strength and acts as a fluid, like when you wiggle your toes in the wet sand near the water at the beach. This effect can be caused by earthquake shaking.

AFTERSHOCKS

Aftershocks are earthquakes that follow the largest shock of an earthquake sequence. They are smaller than the main shock and within 1-2 rupture lengths distance from the main shock. Aftershocks can continue over a period of weeks, months, or years. In general, the larger the main shock, the larger and more numerous the aftershocks, and the longer they will continue.

MAGNITUDE

The magnitude is a number that characterizes the relative size of an earthquake. Magnitude is based on measurement of the maximum motion recorded by a seismograph. Several scales have been defined, but the most commonly used are (1) local magnitude (ML), commonly referred to as "Richter magnitude," (2) surface-wave magnitude (Ms), (3) body-wave magnitude (Mb), and (4) moment magnitude (Mw). Scales 1-3 have limited range and applicability and do not satisfactorily measure the size of the largest earthquakes. The moment magnitude (Mw) scale, based on the concept of seismic moment, is uniformly applicable to all sizes of earthquakes but is more difficult to compute than the other types. All magnitude scales should yield approximately the same value for any given earthquake.

Source: http://earthquakes.usgs.gov/learn/glossary/?alpha=S

2 – EARTHQUAKE RICHTER MAGNITUDE SCALE and CLASSES

EARTHQUAKE RICHTER MAGNITUDE SCALE

RICHTER MAGNITUDE	EARTHQUAKE EFFECTS	EST. NUMBER PER YEAR
2.9 of less	Usually not felt, but can be recorded by seismograph.	1,300,000
3.0 to 3.9	Often felt, but only causes minor damage.	130,000
4.0 to 4.9	Often felt, but only causes minor damage.	13,000
5.0 to 5.9	Slight damage to buildings and other structures.	1,319
6.0 - 6.9	May cause a lot of damage in very populated areas.	134
7.0 to 7.9	Major earthquake. Serious damage.	17
8.0 or greater	Great earthquake. Can completely destroy communities near the epicenter.	1

Source: http://neic.usgs.gov/neis/eqlists/eqstats.html

EARTHQUAKE RICHTER MAGNITUDE CLASSES

Earthquakes are also classified in categories ranging from minor to great, depending on their magnitude.								
CLASS RICHTER MAGNITUDE								
Great	8 or more							
Major	7 - 7.9							
Strong	6 - 6.9							
Moderate	5 - 5.9							
Light	4 - 4.9							
Minor	3 -3.9							

Farth surpluse are also classified in categories ranging from minor to

3 – EARTHQUAKE PROTOCOLS

- When an earthquake occurs, there is no warning; the destruction from an earthquake depends on the magnitude of the quake and the design of structures. Aboveground structures will show various stages of damage reflecting the magnitude of the earthquake.
- What is not obvious is the damage underground facilities may sustain as a result of an earthquake.
- The following pages are minimal protocols that should are put in place after an earthquake has occurred in or near areas with underground facilities served by Oklahoma State University Stillwater Campus.
- Actions to be taken and/or considered are determined by:
 - 1) the magnitude of the earthquake; and,
 - 2) the distance in miles to the nearest OSU Stillwater Facility.
- Depending on the underground piping (cast iron, plastic or steel) in or near the area of the earthquake, more stringent actions may need to be taken to assure underground facilities are safe.
- In the event of an earthquake in the OSU gas system service, the Earthquake Action Log will be completed for the event. The purpose of the Earthquake Action Log is to document the appropriate actions taken, based on the severity of the earthquake and its proximity OSU Stillwater facilities.

Natural Gas - Earthquake Protocol

Oklahama Stata University Stillwator Compus

Earthquake Magnitude 1 - 3		3.1	- 3.9			4.0 - 4.9 5.0 - 5.5 5.6 - 5				- 5.9						
Miles to Nearest Facilities Any	0-10	10-30	30-100	>100	0-10	10-30	30-100	>100	0-10	10-30	30-100	>100	0-10	10-30	30-100	>100
* Actions to be taken and considered							1							1		
No Action x			Х	Х				Х				Х				Х
Monitor Web, App & TV	Х	Х			Х	Х	Х		Х	Х	Х		Х	Х	Х	
Notify UD Supervisor, UD On Call					Х	Х	Х		Х	Х	Х		Х	Х	Х	
Notify FM Work Control					х				х	х			Х	х		
Notify Distribution Manager					Х				Х	Х			Х	Х		
Notify Energy Services Director					х				х	х			х	х		
Send Out UD Patrols					х				Х	Х			Х	х		
nitiate Leak Survey													Х	Х		
Mobilize MEP/Zone On Call													Х	х		
Notify EOC Commander					х								Х	х		
Earthquake Magnitude		6.0 and	l Higher													
Miles to Nearest Facilities	0-10	10-30	30-100	>100		* Definitions of Action to be Taken According to Earthquake Magnitudes										
* Actions to be taken and considered						4 . 0 0 1 1										
No Action						1. OSU	will not re	spond.								
Monitor Web, App & TV	Х	х	Х	Х		2. Utility	/ crew will	monitor w	ebs, apps	and TV.						
Notify UD Supervisor, UD On Call	Х	х	Х	Х		3. Utility	/ superviso	or and on-	call will be	e notified a	and detern	nine actior	n to be tal	ken.		
Notify FM Work Control	Х	х				4. Utility supervisor will notify Work Control for support and awareness.										
Notify Distribution Manager	х	х				5. Utility supervisor will notify manager that a qualifying earthquake has been detected.										
Notify Energy Services Director	Х	х				6. Utility manager will notify director that a qualifying earthquake has been detected.										
Send Out UD Patrols	Х	х				7. Utility	superviso	r will send	l out Distri	bution cre	w to initiat	te patrollir	ıg.			
Initiate Leak Survey	Х	х				8. Utilitie	s supervis	or will initi	ate the lea	ak survey.						
Mobilize MEP/Zone On Call	х	х				9. Utility	supervisor	will reque	est MEP/Z	one On C	all Suppor	t.				
Notify EOC Commander	Х	х				10. Energy Services Director will notify administration for campus EOC support consideration.										
Request Mutual Assistance						11. Energy Services will request the support of mutual aid, ONG, PRC and contract crews.										

L

4 – THE MODIFIED MERCALLI INTENSITY SCALE

The Modified Mercalli Intensity Scale

Earthquake Richter Scale

The Modified Mercalli Intensity Scale of 1931 is the basis for the U.S. evaluation of seismic intensity. Unlike earthquake magnitude, which indicates the energy a quake expends, Mercalli intensity denotes how strongly an earthquake affects a specific place. It has 12 divisions, using Roman numerals from I to XII.

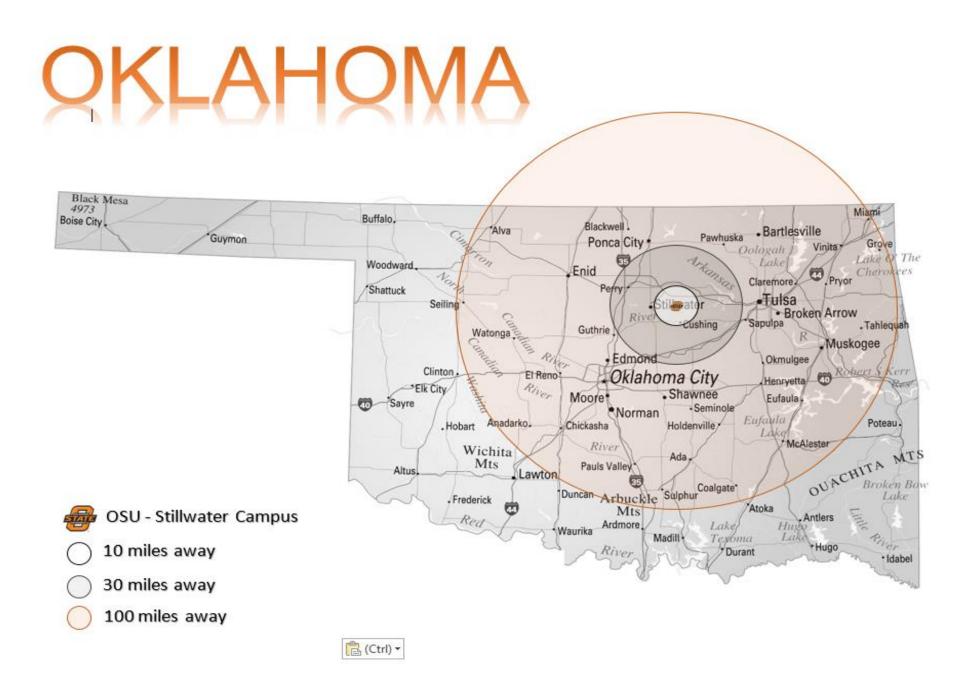
MAGNITUDE	MERCALLI	INTENSITY DESCRIPTION
2	I II	Usually not felt, but detected by instruments. Felt only by a few persons at rest, especially on upper floors of buildings. Delicately suspended objects may swing.
3 III		Felt quite noticeably indoors, especially on upper floors of buildings, but many people do not recognize it as an earthquake. Standing motor cars may rock slightly. Vibration like passing truck.
	IV	During the day felt indoors by many, outdoors by few. At night, some awakened. Dishes, windows, and doors disturbed; walls make creaking sound. Sensation like heavy truck striking building. Standing motorcars rock noticeably.
4	V	Felt by nearly everyone; many awakened. Some dishes, windows, etc., broken; a few instances of cracked plaster; unstable objects overturned. Disturbance of trees, poles, and other tall objects sometimes noticed. Pendulum clocks may stop.
5	VI	Felt by all; many frightened and run outdoors. Some heavy furniture moved; a few instances of fallen plaster or damaged chimneys. Damage slight.
	VII	Everybody runs outdoors. Damage negligible in buildings of good design and construction slight to moderate in well-built ordinary structures; considerable in poorly built or badly designed structures. Some chimneys broken. Noticed by persons driving motor cars.
6	VIII	Damage slight in specially designed structures; considerable in ordinary substantial buildings, with partial collapse; great in poorly built structures. Panel walls thrown out of frame structures. Fall of chimneys, factory stacks, columns, monuments, walls. Heavy furniture overturned. Sand and mud ejected in small amounts. Changes in well water. Persons driving motor cars disturbed.
7	IX	Damage considerable in specially designed structures; well-designed frame structures thrown out of plumb; great in substantial buildings, with partial collapse. Buildings shifted off foundations. Ground cracked conspicuously. Underground pipes broken.
	X	Some well-built wooden structures destroyed; most masonry and frame structures destroyed with foundations; ground badly cracked. Rails bent. Landslides considerable from riverbanks and steep slopes. Shifted sand and mud. Water splashed over banks.
8	XI	Few, if any (masonry), structures remain standing. Bridges destroyed. Broad fissures in ground. Underground pipelines completely out of service. Earth slumps and landslips in soft ground. Rails bent greatly.
	XII	Damage total. Waves seen on ground surfaces. Lines of sight and level distorted. Objects thrown upward into the air.

5 – EARTHQUAKE ACTION LOG

I

EARTHQUAKE ACTION LOG

Date/Time of Notification	
Date:	Time:
Location:	Magnitude:
Facilities Checked OSU Stillwater	
1.	2.
3.	4.
5.	6.
Person Sent to Check Facilities	
Findings	
Action Taken - If Any	
Follow-Up Recommendations/Required	
Pollow-Op Recommendations/ Required	



CHAPTER 19 – NG System Emergency Operations Plan

Oklahoma State University

Stillwater, Oklahoma



Facilities Management - Energy Services Central Plant, Bldg. #0282 - 510 North Washington, Stillwater OK 74078

Distribution Systems Utilities Distribution Natural Gas System EMERGENCY PLAN

Revised November 2024

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EMERGENCY PLAN OVERVIEW

This Emergency Plan provides a guide for complying with the Federal and State requirements, assuring safety for the public and maintaining facilities in satisfactory condition.

An "emergency" condition exists when OSU management, or a responsible person, has determined that extraordinary procedures, equipment, manpower and supplies must be employed to protect the public safety or property from existing or potential hazard.

These hazards will include, but are not limited to, the following:

- Under pressure in the gas system
- Overpressure in the gas system
- Uncontrolled escaping gas
- Fire or explosion near or directly involving a pipeline facility.
- Any leak considered hazardous.
- Danger to major segment(s) of the system

The hazards also include:

- Natural disasters (floods, tornadoes, hurricanes, earthquakes, etc.)
- Civil disturbances (riots, etc.)
- Load reduction conditions (result in voluntary or mandatory reduction of gas usage)

EMERGENCY PROCEDURES

I - Incident Notification

In the event of a natural gas leak that has the potential to represent a hazard to persons or property, move away from the site of the leak and notify 911 immediately.

• <u>911 Emergency</u>--(911)

911 dispatch will gather information from the caller and contact the following appropriate departments:

- Stillwater Fire Department
- OSU Campus Police
- LifeNet EMS
- OSU Facilities Management Work Control (405-744-7154)

Facilities Management Work Control

Work Control personnel (or evening ops), upon receiving the call from 911 dispatch, will immediately report the leak event to the following Oklahoma State University authorities:

Position Title	Name	Office Phone	Cell Phone
DIST SYS Supervisor	Norm Howard	405-744-4412	405-612-5287
DIST SYS Asst. Spvsr.	Josh Page	405-744-4395	321-368-5610
DIST SYS Manager	Greg McKnight	405-744-7288	405-334-7067
Energy Services Director	Brandon Neal	405-744-7149	405-747-4867
OSU Envr. Health & Safety	Kim Southworth	405-744-7241	

II - Incident Priorities and Criteria for Action

A. Priorities

- The first priority of action for all incidents involving natural gas will be directed toward life safety first followed by property. Immediate care shall be given to any injured person(s).
- 2. Determine the Incident Level based upon criteria listed in this outline.
- 3. The surrounding area may be evacuated to reduce the risk of additional casualties.

B. Level 1 Incidents: Leak classification and action criteria.

Level 1 Definition:

A leak that represents an existing or probable hazard to persons or property. Requires immediate repair or continuous action until the conditions are no longer hazardous.

Level 1 Action Criteria:

Requires prompt action to protect life and property, and continuous action until the conditions are no longer hazardous.

Prompt action in some instances may require one or more of the following (not necessarily in this order):

• Notifying police and fire departments by calling 911

- Implementation of OSU Emergency Plan
- Evacuating a suitable area based on the size of the leak.
- Blocking off an area
- Rerouting traffic
- Eliminating sources of ignition
- Venting the area
- Stopping the flow of gas by closing valves or other means

Examples:

- 1. Any leak which, in the judgment of operating personnel at the scene, is regarded as an immediate hazard.
- 2. Escaping gas that has ignited.
- 3. Any indication of gas that has migrated into or under a building or into a tunnel.
- 4. Any underground reading at the outside wall of a building or where gas would likely migrate to an outside wall of a building.
- 5. Any reading of 80% LEL or greater in a confined space.
- 6. Any reading of 80% LEL or greater in small substructures (other than gas-associated substructures) from which gas would likely migrate to the outside wall of a building.
- 7. Any leak that can be seen, heard, or felt, and is in a location that may endanger the general public or property.
- C. Level 2 Incidents Leak classification and action criteria.

Level 2 Definition

A leak that is recognized as being non-hazardous at the time of detection, but justifies scheduled repair based on probable future hazard.

Level 2 Action Criteria

Leaks should be repaired or cleared within one calendar year, but no later than 15-months from the date the leak was reported. In determining the repair priority, criteria such as the following should be considered:

- Amount and migration of gas.
- Proximity of gas to buildings and sub-surface structures
- Extent of pavement
- Soil type and soil conditions (such as frost cap, moisture & natural venting)

Level 2 leaks should be reevaluated at least once every six months until cleared. The frequency of reevaluation should be determined by the location & magnitude of the leakage condition.

Level 2 leaks may vary greatly in degree of potential hazard. Some Level 2 leaks, when evaluated by the above criteria, may justify scheduled repair within the next 5-working days. Others will justify repair within 30-days. During the working day on which the leak is

discovered, these situations should be brought to the attention of the individual responsible for scheduling leak repair.

On the other hand, many Level 2 leaks, because of their location and magnitude, can be scheduled for repair on a normal routine basis with periodic re-inspection, as necessary.

Examples:

- 1. Leaks requiring action ahead of ground freezing or other adverse changes in venting conditions. Any leak that, under frozen or other adverse soil conditions, would likely migrate to the outside wall of a building.
- 2. Leaks requiring action within 6-months.
 - Any reading of 40% LEL, or greater, under a sidewalk in a wall-to-wall paved area that does not qualify as a Level 1 leak.
 - Any reading of 100% LEL, or greater, under a street in a wall-to-wall paved area that has significant gas migration and does not qualify as a Level 1 leak.
 - Any reading less than 80% LEL in small substructures (other than gas-associated substructures) from which gas would likely migrate creating a probable future hazard.
 - Any reading between 20% LEL and 80% LEL in a confined space
 - Any reading on a pipeline operating at 30% SMYS, or greater, in a class 3 or 4 location, does not qualify as a Level 1 leak.
 - Any reading of 80% LEL, or greater, in gas-associated substructures
 - Any leak that, in the judgment of operating personnel at the scene, is of sufficient magnitude to justify scheduled repair.
- D. Level 3 Incidents Leak classification and action criteria

Level 3 Definition:

A leak that is non-hazardous at the time of detection and can be reasonably expected to remain non-hazardous.

Level 3 Action Criteria:

These leaks should be re-evaluated during the next scheduled survey, or within 15-months of the date reported, whichever occurs first, until the leak is re-graded or no longer results in a reading.

Examples:

Leaks requiring re-evaluation at periodic intervals:

- Any reading of less than 80% LEL in small gas-associated substructures
- Any reading under a street in areas without wall-to-wall paving where it is unlikely the gas could migrate to the outside wall of a building.
- Any reading of less than 20% LEL in a confined space

III - Incident Responsibilities

- 1. The 1st Responder shall establish a unified command post (utilizing the Incident Command System) near the scene, when necessary or required, to coordinate the incident.
- 2. On-scene emergency personnel from LifeNet EMS shall provide immediate first aid to injured persons when it is safe to do so.
- 3. OSU Campus Police and Stillwater Fire Department shall conduct evacuations in the event of fire, explosion, natural disaster or other type of incident, when necessary, as directed by the Incident Commander.
- 4. OSU Campus Police, in conjunction with other supporting agencies, shall establish, maintain, and man all necessary incident perimeters and barricades as directed by the Incident Commander.
- 5. OSU Energy Services personnel shall isolate the incident area by shutting off the flow of any gas from feed lines into the impacted area, only after the determination that such action can be performed safely.
- 6. The City of Stillwater Fire Department shall manage any fire suppression needs and may assist LifeNet EMS in providing advanced emergency medical care and transportation of patients.
- 7. Manpower and equipment shall be provided by OSU's Facilities Management at the request of the Incident Commander.

IV - Response Procedures

In case of fire located near or directly involving a pipeline facility, explosion occurring near or directly involving a pipeline facility, natural disaster, or other emergency incident, the following response procedures will be followed:

Notification will proceed as designated on page-5 of this document.

The first responder(s) shall designate an incident commander and activate the incident command system (ICS). When necessary, an on-scene incident command post shall also be established.

The on-scene incident command post shall be located upwind and as close as practical to the incident site so that continual visual observations may be maintained of the incident area, and immediate response to changing conditions may be possible. The on-scene command post shall stay in communication with all responding agencies.

Responding agencies shall provide designated responsibilities as listed above, under the direction of the incident commander.

First aid and medical care will be provided by LifeNet EMS to injured persons as soon as possible.

Firefighting and fire suppression operations will be initiated and conducted by Stillwater Fire Department.

Gas valve shut off will be conducted as quickly as possible by OSU Energy Services department, once the determination is made that it is safe to do so.

Perimeter zone(s) around the affected area shall be established as directed by the incident commander in accordance with standard emergency scene practices.

Hazard Zone - The Hazard Zone is the area in which personnel are potentially in immediate danger from the hazardous situation. This zone shall be established by the incident commander. Access to this area will be rigidly controlled and only authorized personnel with proper protective equipment and an activity assigned by the Energy Services, Distribution Systems Manager or his representative and approved by the on-site incident command post shall be allowed to enter the incident area. OSU Campus Police personnel will be assigned to monitor the entry and exit of all personnel from the Hazard Zone.

Evacuation Zone - The Evacuation Zone is the larger area surrounding the Hazard Zone, in which a lesser degree of risk to emergency personnel exists, but from which all civilians will be removed. The limits of this zone will be enforced by the OSU Campus Police and other agencies based upon distances and directions established by the incident commander. The area to be evacuated depends upon the nature and extent of the fire, explosion, natural disaster, or other emergency. All evacuations shall be ordered by the incident commander and shall be conducted in an orderly, expedient fashion.

Additional Perimeter Zones may be established, as necessary. These may include Hot Zone, Warm Zone, and Cold Zone for gas incidents that may also involve hazardous chemicals, as well as a Staging Area for any major incident that may require large numbers of personnel and equipment.

Incident-specific circumstances will dictate other procedures that will be used to bring the emergency under control in accordance with the priorities of life safety first, followed by the protection and salvage of property.

V - POST Incident Management

- A. Upon declaration of the Incident Commander that the incident is under control and the incident area is safe, Stillwater Fire Department personnel shall sweep the incident area searching for any additional casualties. Upon completion of the sweep, responsible personnel shall begin the cause and origin procedures. Upon completion of the investigation, repairs may be initiated.
- B. Barriers shall remain intact, and any area vacated due to the incident shall remain vacated until repairs and any required tests are completed before restoring all systems back to normal operating conditions.

- C. Repairs shall be initiated immediately and shall be expedited to restore normal service and to place OSU's gas distribution system into a normal and safe mode of operation.
- D. Normal procedures shall apply to the emergency repairs:
 - 1. Only qualified OSU personnel shall perform the repairs.
 - 2. Only approved material as specified in the Guide for Small Gas Operators shall be utilized.
 - 3. OSHA & OSU's safety procedures and guidelines shall be utilized.
- E. Upon completion of repairs, and after the gas system has been successfully tested and restored to operation, the incident area may be released for normal operation.
 - 1. A final inspection of the area shall be conducted by qualified personnel at the direction of the Incident Commander.
 - 2. As directed the Incident Commander:
 - Barriers shall be removed.
 - Personnel shall be allowed to return to the area.
 - Emergency personnel shall be released upon direction by the Incident Commander

VI - POST Incident Reporting

- A. The University Fire Marshal, shall, within 72-hours of the closure of the Level One incident, schedule and facilitate a debriefing with all agencies concerned, i.e., University, City, State, ONG, and National participants. This debriefing shall include, but not be limited to:
 - 1. Critique of the incident
 - 2. Problem areas identified.
 - 3. Revisions to the emergency plan, if needed
 - 4. Factors that caused the incident
- B. Upon completion of the debriefing, open discussion for questions and answers.
- C. The University Fire Marshal issues the final report.

RESPONDING to GAS LEAK REPORTS

It is the responsibility of OSU Facilities Management to train its employees on policy and procedure concerned with gas leak calls and reports.

- I. The Facilities Management (Work Control) employee receiving a report of a gas leak should get as much of the information as possible to fill out a leak report, or Facilities Management Work Request.
- II. All reports of gas leaks on OSU property are assigned a high priority. Leaks inside a facility or building receive a Priority One.
- III. Upon receiving pertinent information, and determining that a hazardous leak exists inside a building, the caller should be advised on the following:
 - a. Do not operate (do not turn on or off) any electrical appliance or device.

- b. Extinguish all open flames. Do not light any matches, cigarettes, etc.
- c. Turn off the gas supply (only if the caller knows how to do so).
- d. Evacuate the building to a safe distance. Be close enough to relay information to arriving emergency personnel.
- IV. Dispatch necessary Facilities Management personnel to the location.
- V. Duties of the first responsible University responder (Facilities Management employee or Campus PD) on the scene: *Take any corrective action necessary to ensure protection of life, then property*. It is the responsibility of the person in charge to:
 - a. Set up communication.
 - b. Coordinate the operation.
 - c. Make all decisions concerning closing emergency valves and isolating areas, as well as coordinate emergency personnel and equipment.

MINIMUM OPERATOR RESPONSE ACTIONS:

- I. Leaks outside of buildings:
 - a. Assess danger to passersby, surrounding buildings and their occupants, and other property.
 - b. Extinguish all open flames.
 - c. If necessary, notify the Stillwater Fire Department.
 - d. Block the street(s)
 - e. Notify the Supervisor or other responsible persons.
 - f. Check neighboring buildings for gas vapors, fumes, etc.
 - g. Implement Check List for major emergency (see page 14).
 - h. Repair leak
 - i. Upon completion of repairs, check the area using a Combustible Gas Indicator; if determined safe, allow occupants to return to the building.
- II. Leaks inside a building:
 - a. Evaluate the issue to determine hazard, concentration of gas, and source of the leak.
 - b. Evacuate the building if required.
 - c. Do not operate any light switches or electrical appliances.
 - d. Do not use the telephone; turn off pagers and cell phones.
 - e. Shut off the gas meter valve.
 - f. Ventilate the building.
 - g. Bar hole the area, especially around the foundation. Check the water meter and other ground openings.
 - h. If the ground is gas-free, and if the building is gas-free, turn on the meter valve. CHECK ALL GAS PIPING AND APPLIANCES FOR LEAKS.
 - i. Implement Check List for major emergency (see page 14).
 - j. Repair leak.
 - k. If leak cannot be repaired, notify Supervisor. Turn off the meter, lock it and tag it out.

III. Gas burning inside a building:

- a. Call 911.
- b. If fire is at the appliance, shut off the gas appliance valve, if possible.
- c. If not possible, shut the gas off at the meter or appropriate valve.
- d. Implement Check List for major emergency (see page 14).

IV. Interruption in the gas supply

An interruption in gas supply could be due to - freezing of the regulators, break in the line, sabotage, or ONG cut-off.

- a. Call OSU's supplier (ONG).
- b. Locate the leak; inform ONG of the location of the leak.
- c. Close appropriate valve in the system to isolate the break.
- d. Implement Check List for major emergency (see page 14).

NG EMERGENCY NOTIFICATION LIST

SYSTEM OWNER: Oklahoma State University

Norm Howard	Norm Howard ES UTIL Distribution Supervisor		405-612-5287
Josh Page ES UTIL Distribution Asst. Supervisor		405-744-4395	321-368-5610
FM Work Control		405-744-7154	
Greg McKnight	ES Distribution Systems Manager	405-744-7288	405-334-7067
Brandon Neal	ES Director	405-744-7149	405-747-4867
Jerry Petre	University Fire Marshal	405-744-1700	405-338-0224
Casey Romero	ES Asst. Director and Energy Management Manager	405-744-4628	

AVAILABLE EMERGENCY EQUIPMENT LIST

EQUIPMENT	AMOUNT	LOCATION	INSPECTION
Backhoe/front-end loader	2	Facilities Management	After 500 hours
Dump trucks	1	Facilities Management	Quarterly
Winch truck	1	Facilities Management	Quarterly
Emergency generators	8	Facilities Management	Monthly
Emergency lights	15	Facilities Management	Monthly
Hand tools	various	Facilities Management	Monthly
Repair kits	2	Facilities Management	Monthly
Barricades/Barriers	numerous	Facilities Management	Monthly
Gas Detectors	7	Facilities Management	Weekly and before each use
Labor	as needed	Call Out	

NOTIFICATIONS LIST

AGENCY

TELEPHONE

LOCAL:

W. Anthony Gillilan, Captain Public Safety Officer	744-4230
Campus Police Dispatcher	744-6523
Stillwater Police Department	372-4171
Stillwater Fire Department	372-0497
Ambulance, Life-Net	707-0060
Emergency Response	911
Oklahoma Natural Gas	405-707-5621

STATE:

Oklahoma Corporation Commission	1-405-521-2258
Pipeline Safety	24 hours
Oklahoma Natural Gas	800-458-4251 24 hours

NATIONAL:

National Response Center1-800-424-8802
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CHECK LIST (MAJOR EMERGENCY)

1. Has 911 Emergency been called? 2. Have the occupants been evacuated to a designated area and the area secured? Has the Police Department been notified by 911 dispatch? 3. 4. Has Life-Net EMS been notified by 911 dispatch? 5. Has a repair crew been notified by Facilities Management Work Control? 6. Has the leak been shut off or brought under control by FM Energy Services? 8. Has the University call list been executed? 9. Has outside help been requested? 10. If an area has been cut off from a supply of gas, has the individual building been cut off? 11. Is the situation under control and has the possibility of recurrence been eliminated? 12. Has the surrounding area, including adjacent buildings and cross streets, been probed for the possibility of further leakage? 14. If applicable, has a telephone report been made to the State? 15. If applicable, has telephonic report been made to NRC/DOT?

REPORTING REQUIREMENTS

- A. A telephone call from a senior University official MUST BE MADE TO THE U.S. DEPARTMENT OF TRANSPORTATION and OKLAHOMA CORPORATION COMMISSION for any leak where:
 - 1. There is a release of gas from a pipeline.

<u>AND</u>

There is a death or personal injury requiring hospitalization or there is estimated property damage, including the cost of gas lost, by the operator or others, of \$145,500 or more.

- 2. There is an event that is significant in the judgment of the operator, even though it was not described in A-1.
- B. A telephone call MUST BE MADE TO THE OKLAHOMA CORPORATION COMMISSION for any leak where:
 - 1. There is a release of gas from a pipeline.

<u>AND</u>

There is a death or personal injury requiring hospitalization or there is estimated property damage, including the cost of gas lost, by the operator or others, of \$5,000 or more.

2. There is an event that is significant in the judgment of the operator, even though it was not described in B-1.

The telephone report to DOT and OCC should contain:

- OSU's address
- Name and phone number of individual reporting the incident.
- The location of the leak (city, county, state, and street address).
- The time of the leak (hour and date).
- The number of fatalities and personal injuries, if any.
- Type and extent of property damage.
- Description of the incident. (See DOT Incident Form, attached.)

A telephonic report should be made at the earliest practicable time following discovery (within 2 hours).

RESTORATION OF GAS SERVICE DUE TO OUTAGE

When the supply of gas has been cut off to an area, the gas should not be restored to the affected area until the individual gas services in a university building have been turned off.

In restoring service on the University to an affected area, all gas piping and meters must be purged and appliances re-lighted. Never turn the gas on at a meter unless you have access to ALL appliances or equipment on the piping.

The OSU Facilities Management person in charge is to coordinate this operation and be responsible for same.

A complete record of the incident, including service restoration and drawings, if necessary, must be kept on file.

EDUCATION AND/OR TRAINING

Employee Training

OSU Facilities Management employees must be trained annually in emergency procedures that include but are not limited to:

- 1. Update of the emergency plan
- 2. Review of employee responsibilities in an emergency
- 3. Review of location and use of emergency equipment.
- 4. Review properties of natural gas.
- 5. Review the locations of:
 - Systems map.
 - Main records
 - Service records
 - Valve records
 - Regulator station schematics
- 6. Take a hypothetical emergency situation and conduct a step-by-step review with employees on the action to be taken, including contact with public officials, Stillwater Fire Department, OSU & Stillwater Police, and ONG, etc.
- 7. Record keeping
- 8. Telephone reports (U.S. DOT, State agency, etc.)
- 9. Records shall be kept on file of attendance and items discussed.
- 10. Liaison with appropriate fire, police, and other public officials.

PUBLIC EDUCATION

Oklahoma State University will, through its Communications Office, enable faculty, staff, students, the general public and appropriate governmental organizations, to recognize a gas emergency. OSU will, through Residential Life, and other departments, instruct the concerned constituency in reporting gas odors, leaks and other emergencies to OSU Facilities Management Work Control, OSU Police, or ONG (Oklahoma Natural Gas).

The program material should include, but not be limited to:

- Information about gas properties
- Recognition of gas odors
- What to do and not do when there is a strong gas odor
- Notification of the University and gas company prior to making excavation-related activities.
- Telephone numbers for persons in the University to report gas leaks or odors or other information during both business and non-business hours.

This information may be conveyed to the University constituency by a number of means:

- Radio and television
- Newspaper
- Meetings
- Bill stuffers
- Mailings
- Hand-outs
- Posted on bulletin boards.
- Employee newsletters
- Campus websites
- Apartment handbooks
- New-employee orientation
- Campus-wide email
- Facilities Management Website

The University will maintain records of the public information program and related activities.

LIAISON WITH PUBLIC OFFICIALS & LOCAL GAS UTILITIES

Environmental Health and Safety will establish liaison with fire, police, civil defense, and medical officials with respect to these emergency procedures. These officials include representatives of Stillwater Police and Fire Departments (911 dispatch management), Payne County Emergency Management and Oklahoma Natural Gas, Life-Net EMS and OSU Student Health Center, as well as OSU Facilities Management managers.

Liaison will consist of annual meetings to discuss what each agency can do for the other to control an emergency situation at the OSU facility. This meeting will be performed with face-to-face communication, at which time a copy of this Emergency Plan will be provided to each official.

Documentation must be kept of all meetings, training sessions, and other related activities, such as:

- Date of meeting, attendance, and titles of participants
- Training sessions on proper procedures to follow during a gas emergency.
- Meetings to learn capabilities, responsibilities, and procedures respecting gas emergencies of each group.

INFORMATION TO THE NEWS MEDIA

During an emergency, refer all requests for information to the University's Communications Office (CO). The CO will coordinate emergency information with responsible OSU management. The OSU plan for public announcements includes:

- Calm the situation.
- Do not make unwarranted comments.
- Tell precisely what the public can do to help.
- Tell specifically what OSU and ONG are doing about the incident.
- Give facts to prevent baseless rumors.
- Repeat the most encouraging view of situation that facts will permit.
- Do not speculate regarding the situation in the absence of facts.

ACCIDENT INVESTIGATION

OSU will proceed in analyzing accidents and failures, and at the minimum:

- Evaluate the situation.
- Protect life and property.
- Keep the area safe.
- Conduct a leak survey.
- Conduct pressure test of piping.
- Perform meter and regulator checks.
- Question persons on the scene
- Examine burn and debris patterns.
- Request ONG test odorization level.
- Record weather conditions.
- Select samples of the failed facility or equipment or equipment for laboratory examination for the purpose of determining the causes of the failure and minimizing the possibility of recurrence
- Notify the appropriate Risk Management Office

TELEPHONIC REPORTS to the FEDERAL GOVERNMENT

Gas pipeline incidents that meet the reportable state requirements and have caused estimated damages in excess of \$50,000 (total of operator's damage and damage to others and including cost of gas loss) must also be reported to the federal government.

 TELEPHONE TOLL FREE
 (800) 424-8802

 WASHINGTON, D.C.
 (202) 426-2675

 24 HOURS EVERY DAY
 (202) 426-2675

This telephonic report, if required, should also be made upon discovery, but in no case later than two hours after discovery. This telephonic report of a serious incident should include:

- Identity of reporting operator,
- Name and phone number of individual reporting the incident,
- The location of the leak (city, county, state, and street address),
- The time of the leak (date and time)
- The number of fatalities and personal injuries, if any,
- Type and extent of property damage, and
- Description of the incident.

EMERGENCY EQUIPMENT

We are responsible for the adequacy, availability, and condition of emergency equipment. Inspection of emergency equipment will be conducted quarterly, or as often as may be necessary, and records of these inspections will be kept on file.

CONTRACTOR EMERGENCY CALL LIST

Contractor's name:

Address: _____

24-hour telephone number:

FACILITY NAME: _____

EMERGENCY PLAN - STAFF TRAINING RECORD

Plans will be reviewed annually, and records of review and training shall be kept on file. Employees shall be trained in the operation/maintenance and emergency plan once each calendar year.

ANNUAL PLAN REVIEW	PERSONNEL TRAINING

INCIDENT REPORT – GAS DISTRIBUTION SYSTEM

Incident Report includes the following two pages.

S Department of Transportation Research and Special Programs Administration INCIDENT REPORT GAS DISTRIBUTION SYSTEM Date of Re				Date of Report
PART 1 - GENERAL REPORT INFORMATION				
 a. Operator's 5-digit identification number: <u>//////</u> b. Name of Operator 		4.	Reason for Reporting □ Fatality persons	Number <u>/ / / /</u>
c Number & Street d.			 Injury requiring inpatient hospitalization persons 	Number
City, County, State, Zip Code			□ Property damage/loss	Estimate \$
2. Location of incident				
a Number & Street			Operator Judgment/Emer	rgency Action
b.			□ Supplemental Report	
City & County		5.	Elapsed time until area was made safe:	<u>///</u> hr. <u>///</u> min.
c		6.	Telephonic Report: /// mo	o. <u>///</u> day <u>///</u> year
d. Class Location □1 □2 □3 □4		7.	a. Estimated pressure at po (PSIG)	int & time of incident
e. Incident on Federal Land? □Yes □No				
3. Time and Date of Incident			b. Maximum allowable oper (PSIG)	
<u>/////</u> hour <u>///</u> mo <u>///</u> day <u>///</u> year			c. MAOP established by:	
			(1) 🛛 Test pressure (PS	SIG)
			(2) 🛛 49 CFR § 192.619	9(a)(3)
PART 2 - APPARENT CAUSE	l _			
□ Corrosion □ Damage by Outsid (continue in Part A) (continue in Part B) □ Other	e Forces	cause	nstruction/Operating Error ed by operator <i>inue in Part C)</i> or C)	□ Accidentally (continue in Parts B
PART 3 - NARRATIVE DESCRIPTION OF FACTORS C			,	h additional sheet(s) as
			1160633	sary)
PART 4 - ORIGIN OF THE INCIDENT				
1. Part of System Where Incident Occurred Image: Main Image: Meter Set Assen Image: Service Line Image: Other 3. Material Involved: Image: Other Image: Steel Image: Cast iron Image: Polyethylene plastic Image: Other Image: Other Other Image: NPS (Nominal Pipe Size) / /// / in. Manufactor 4. Specification Manufactor	Wall Thickness	///// in.	□ Regulator/meter □ Joint, type □ Weld	ongitudinal, fillet)
PART 5 - ENVIRONMENT				
Area of Incident □ Within/Under Building □ Under Pavement □	Above Ground	Under Ground or	Under Water	
PART 6 - PREPARER AND AUTHORIZED SIGNATURE				
Preparer's Name & Title - PRINT			Telephone Number	
Authorized Signature & Date			Telephone Number	

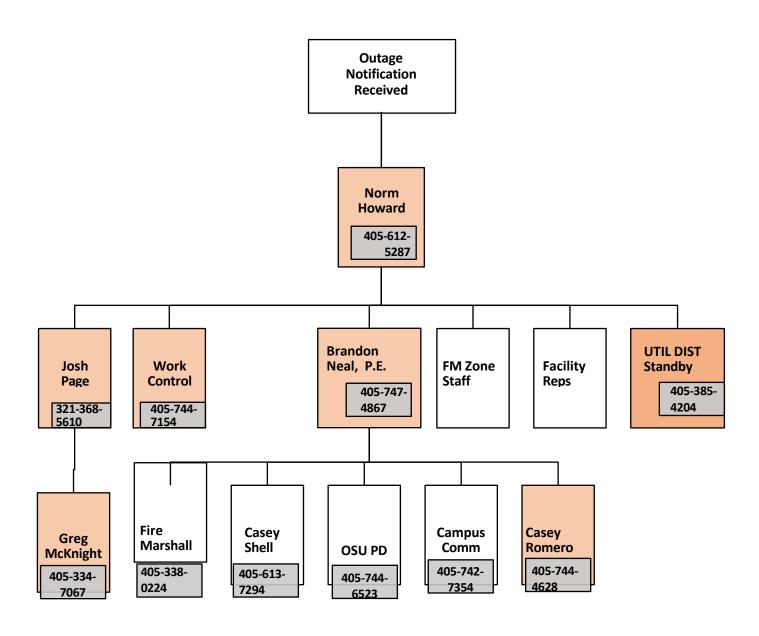
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INCIDENT REPORT -- GAS DISTRIBUTION SYSTEM (continued)

PAI	RT A - CORROSION					
1.	Where did the corrosion occur? Internally Externally	2.	Visual Description Localized Pitting General Corrosion Other	3.	Cause Galvanic Other	
4.	Pipe Coating Information □ Bare □ Coated					
5.	Was corroded part of pipeline consi Yes Year protection started / No		er cathodic protection prior to disco	overing incident?		
6.	Additional Information:					
PAI	RT B - DAMAGE BY OUTSIDE FOR	CES				
1.	Primary Cause of Incident Damage resulted from action of Damage resulted from action by Damage by earth movement Subsidence Landslide/Washout Frost Other Damage by lightning or fire					
2.	 2. Locating information (for damage resulting from action of outside party/third party) a. Did operator get prior notification that equipment would be used in the area? Yes Date received /// mo. /// day /// yr. No b. Was pipeline location marked either as a result of notification or by markers already in place? Yes Permanent Markers Temporary Stakes Other No c. Does Statute or ordinance require the outside party to determine whether underground facility(ies) exist? Yes No 					
3.	Additional Information:					
PAI	RT C - CONSTRUCTION DEFECT					
1.	Cause Poor workmanship during constr Physical damage during constru		erating procedures inappropriate er		g procedure application	
2.	Additional information:					
PAI	RT D - OTHER					
Brie	f Description:					

NOTICE: This report is required by 49 CFR Part 191. Failure to report can result in a civil penalty not to exceed \$1,000 for each violation for each day that such violation persists except that the maximum civil penalty shall not exceed \$200,000 as provided in 49 USC 1678.

NG OUTAGE COMMUNICATION TREE



Primary Roles (mandatory notification)

If the next person in a primary role cannot be reached, take responsibility to call the next level of primary roles. If anyone in the middle of the tree receives the first notification, notify the primary role above and respective roles below.

M:\DIST SYSTEMS\UTIL DIST\NATURAL GAS\NG MANUAL\FY25_NG-MANUAL\NG-MANUAL-BODY_Revision_FY25.docx

CHAPTER 20 – OSU Stillwater Natural Gas MAP

Link to the GIS map is: https://fm-gis-portal.okstate.edu/portal/apps/utilitymapviewer/#